

# 13\_1 Geothermal - GSHPs

## Recap:

### 1. Direct Use:

- Utilizes low heat/quality resource to fill a significant need
- Potentially utilizes the ~50% rejected heat in the Sankey diagram

Movies: (Great Lakes SedHeat Network): <https://igws.indiana.edu/glsn/speakers>

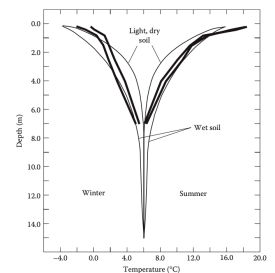
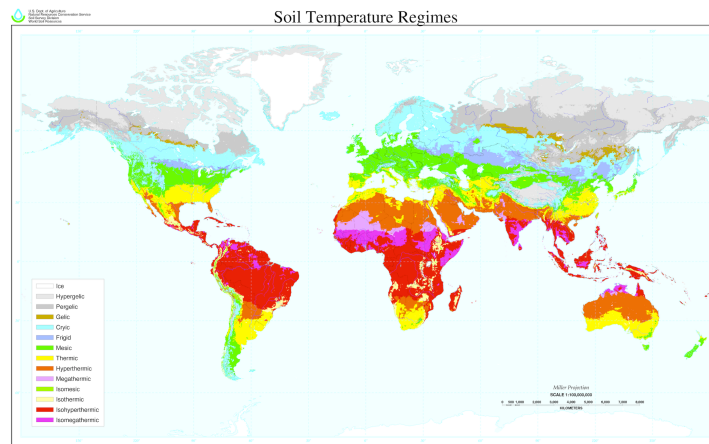
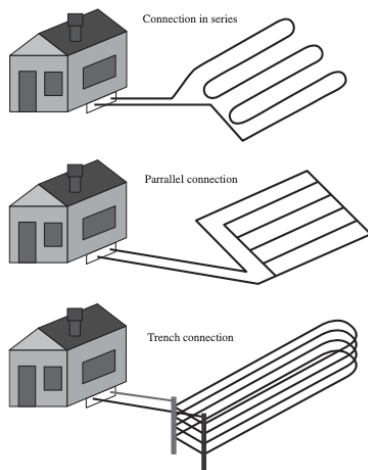
(Jerrod): [https://personal.ems.psu.edu/~fkd/courses/eme\\_497/videos/3\\_v\\_anthonjjerrod.mp4](https://personal.ems.psu.edu/~fkd/courses/eme_497/videos/3_v_anthonjjerrod.mp4)

(Shreya): <https://drive.google.com/file/d/1MuDdfXslJnNfs1g8YcSj5PVVkrDgfZ5v/view>

Resources: WG11 & MR 5+6

## Motivation:

**1. Motivation [10%]** Provide context for the topic. *Use of relevant public domain videos* are a useful method for this. Why is this particular topic or sub-topic important in the broad view of geothermal energy engineering?



Soil Map: [https://www.nrcs.usda.gov/wps/portal/nrcs/detail/soils/use/worldsoils/?cid=nrcs142p2\\_054019](https://www.nrcs.usda.gov/wps/portal/nrcs/detail/soils/use/worldsoils/?cid=nrcs142p2_054019)

Utilize low quality heat without the penalty of conversion to electricity  
Distributed power opportunity for off-grid and remote use  
Broadly geographically available (in US) due to climatic zonations

## Scientific Questions:

**2. Scientific Questions to be Answered/Outline [10%]** What questions arise from the motivation. What are the sub-topical areas that address these scientific questions.

## GSHPs

- Mechanisms of heat flow in the shallow earth?
- Mechanism of utilizing low quality heat -> high(er) quality heat?
- Rate-limiting processes?

# 1. Mechanisms of heat flow in the shallow earth?

**TABLE 11.2**  
**Thermal Conductivity (W/m-K) and the Constant Pressure Heat Capacity ( $C_p$  [J/mole-K]) of Some Common Materials at 25°C**

Material	$k_{th}$	$C_p$	$Q$	$m^3$
Quartz <sup>a</sup>	6.5	44.5	1960	128.5
Alkali feldspar <sup>a</sup>	2.34	203	2000	130
Calcite <sup>a</sup>	2.99	82	2103	120
Kaolinite <sup>a</sup>	0.2	240	2408	105
Water	0.61	75.3	4181	60

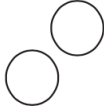
Source: <sup>a</sup>  $C_p$  computed from Helgeson, H.C. et al., *American Journal of Science*, 278-A, 229, 1978.

Note: The amount of heat,  $Q$  (kJ/m<sup>3</sup>-K), that must be supplied or removed, per cubic meter of material, for 1°C of temperature increase or decrease at about 25°C is shown. The number of cubic meters of each material needed to supply 7 kW of heat is shown in the column  $m^3$  (see text for details).

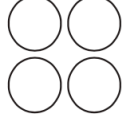
$$Q = \rho C_p \Delta T \cdot V$$

Note: Use J/kg.K

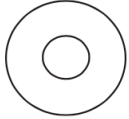
Simple U-tube



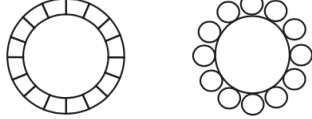
Double U-tube



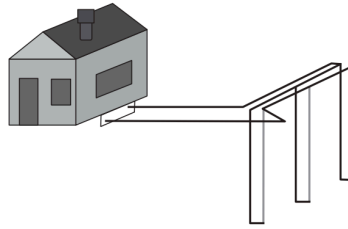
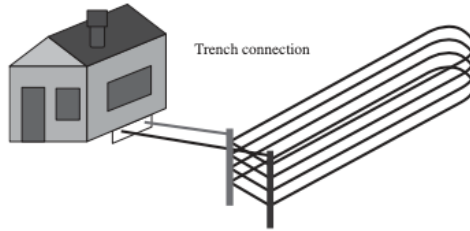
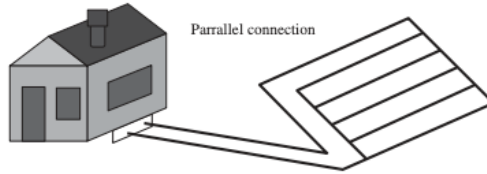
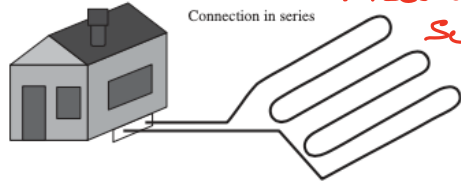
Simple coaxial



Complex coaxial

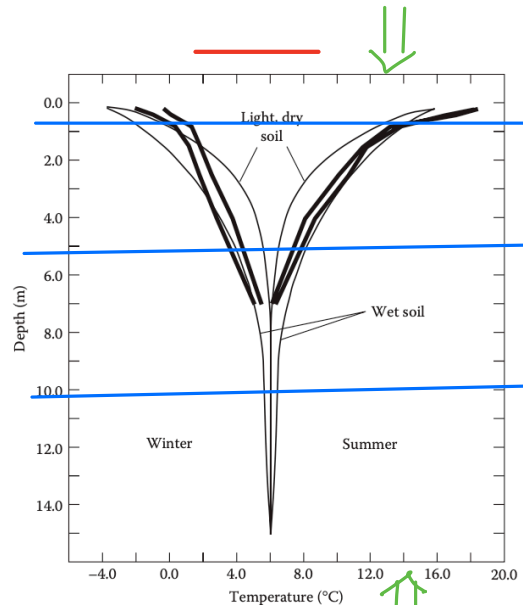
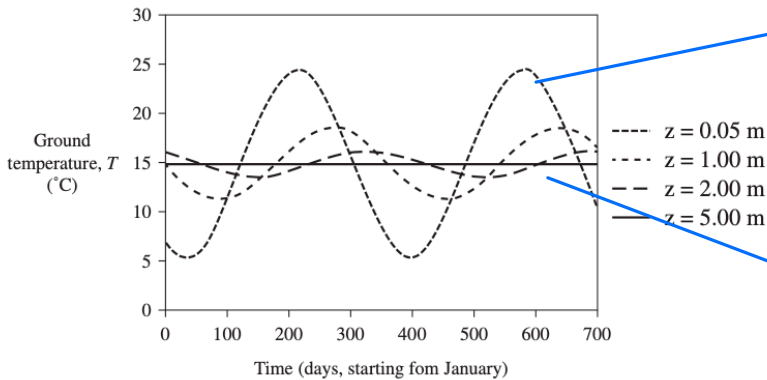


RECOVER HEAT FROM SHALLOW SUBSURFACE



This defines amount of heat supplied but not the RATE.

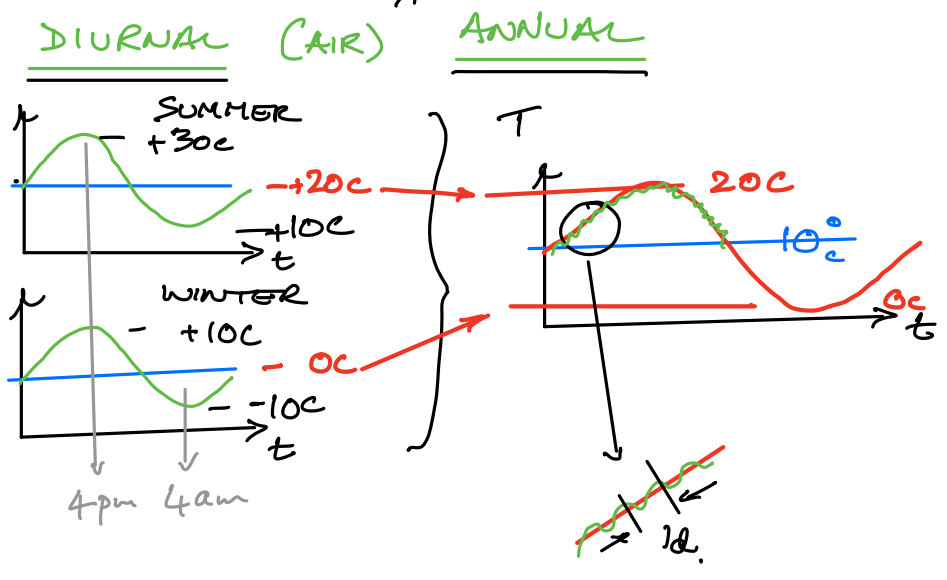
INSOLATION 200 - 1500 W/m<sup>2</sup>



GEOTHERMAL FLUX = 87 mW/m<sup>2</sup>

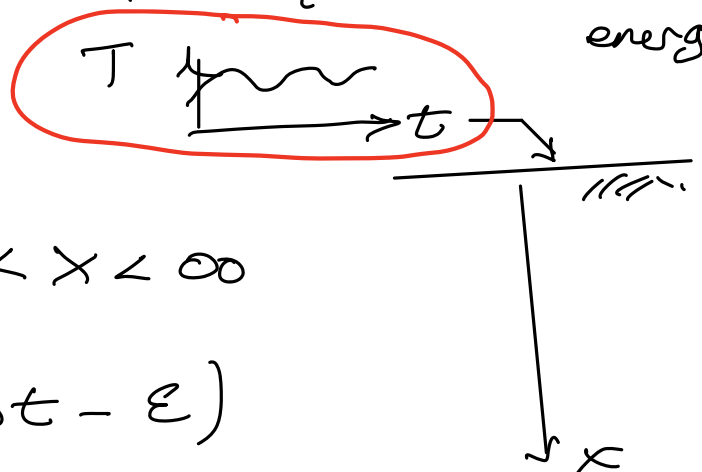
# TEMPERATURE CHANGES IN SHALLOW SUBSURFACE

$200 \text{ W/m}^2 \gg 87 \text{ mW/m}^2$   $\therefore$  Insolation dominates  
 Insolation  $\quad$  Geothermal  $\quad$  - sets deep temperature as average



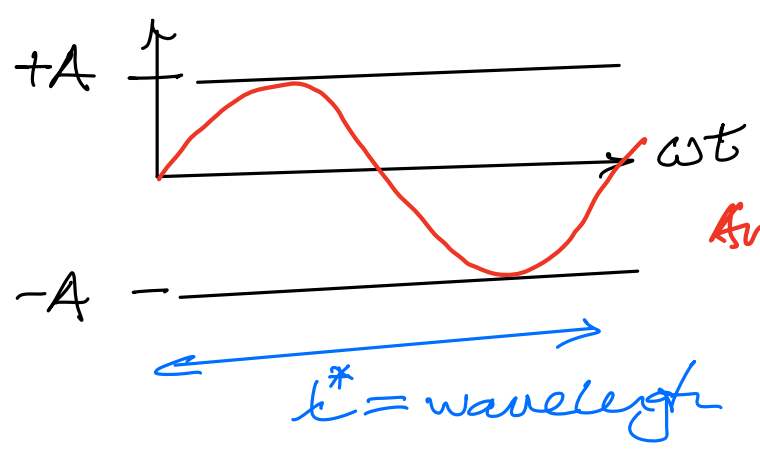
Solve:  $\rho c \frac{\partial T}{\partial x} = \lambda \frac{\partial^2 T}{\partial x^2}$

- 1. Fourier's Law
- 2. Conservation of energy



ICs:  $T=0 \quad 0 < x < \infty$

BCs:  $T = A \cos(\omega t - \epsilon)$



Amplitude =  $A \doteq K \text{ or } C$

Ang. Frequency =  $\omega \doteq \frac{1}{\text{sec}}$

$n = \text{frequency} = \frac{\omega}{2\pi}$

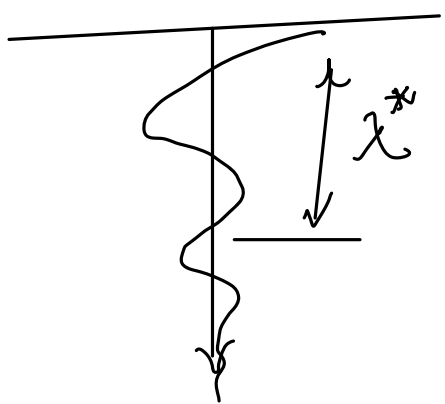
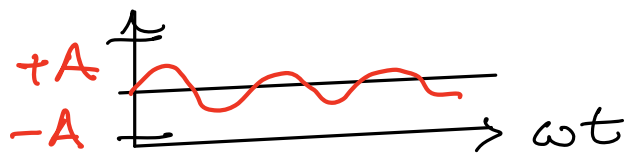
# SOLUTION (dynamic steady state)

$$T = A e^{-kx} \cos(\omega t - kx - \epsilon)$$

with  $k = \left(\frac{\omega}{2K}\right)^{1/2} = \text{wave number} = \frac{1}{m}$

$$K = \frac{\lambda}{\rho c} = \text{thermal diffusivity} \quad \text{m}^2/\text{s}$$

Wavelength (in space not time  $\omega t$ )



$$\lambda^* = \frac{2\pi}{k} = \frac{4\pi K}{n}$$

and  $n = \text{frequency} = \frac{\omega}{2\pi}$

Set  $kx = 2\pi$  (i.e. one wavelength)

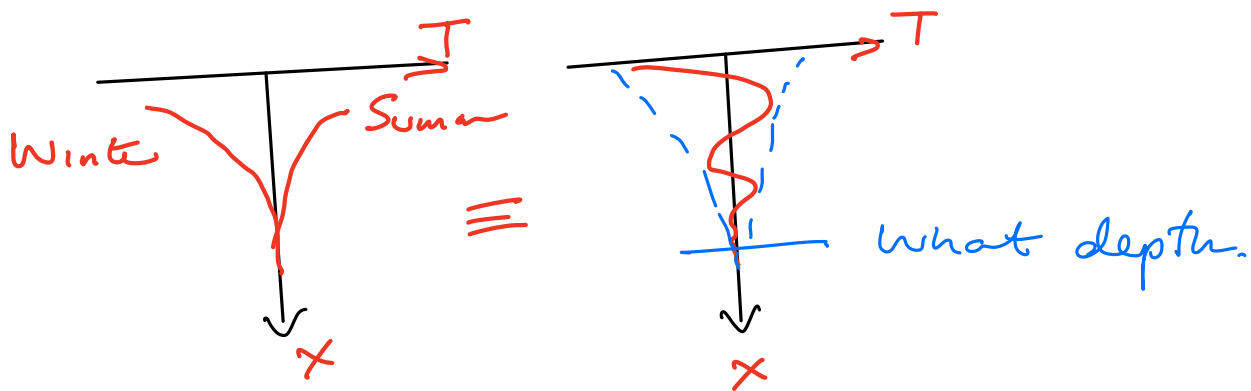
Then  $2\pi = kx = \left(\frac{\omega}{2K}\right)^{1/2} x$     &  $\omega = 2\pi n$

$$2\pi = \left( \frac{2\pi n}{2K} \right)^{1/2} x$$

$$\text{or } x = (2\pi)^{1/2} \cdot \left( \frac{2K}{n} \right)^{1/2}$$

$$x = \left( \frac{4\pi K}{n} \right)^{1/2} = \lambda^* \leftarrow$$

Depth for no temperature change



$$T = A e^{-kx} ( )$$

$$\text{And } e^{(-2\pi)} \approx 0.0019 \approx 0.002$$

$$\approx 0.2\% \approx 0$$

$$-2\pi = -kx \quad \therefore \quad x = \left( \frac{4\pi K}{n} \right)^{1/2}$$

If  $K = 30 \text{ m}^2/\text{yr}$ .

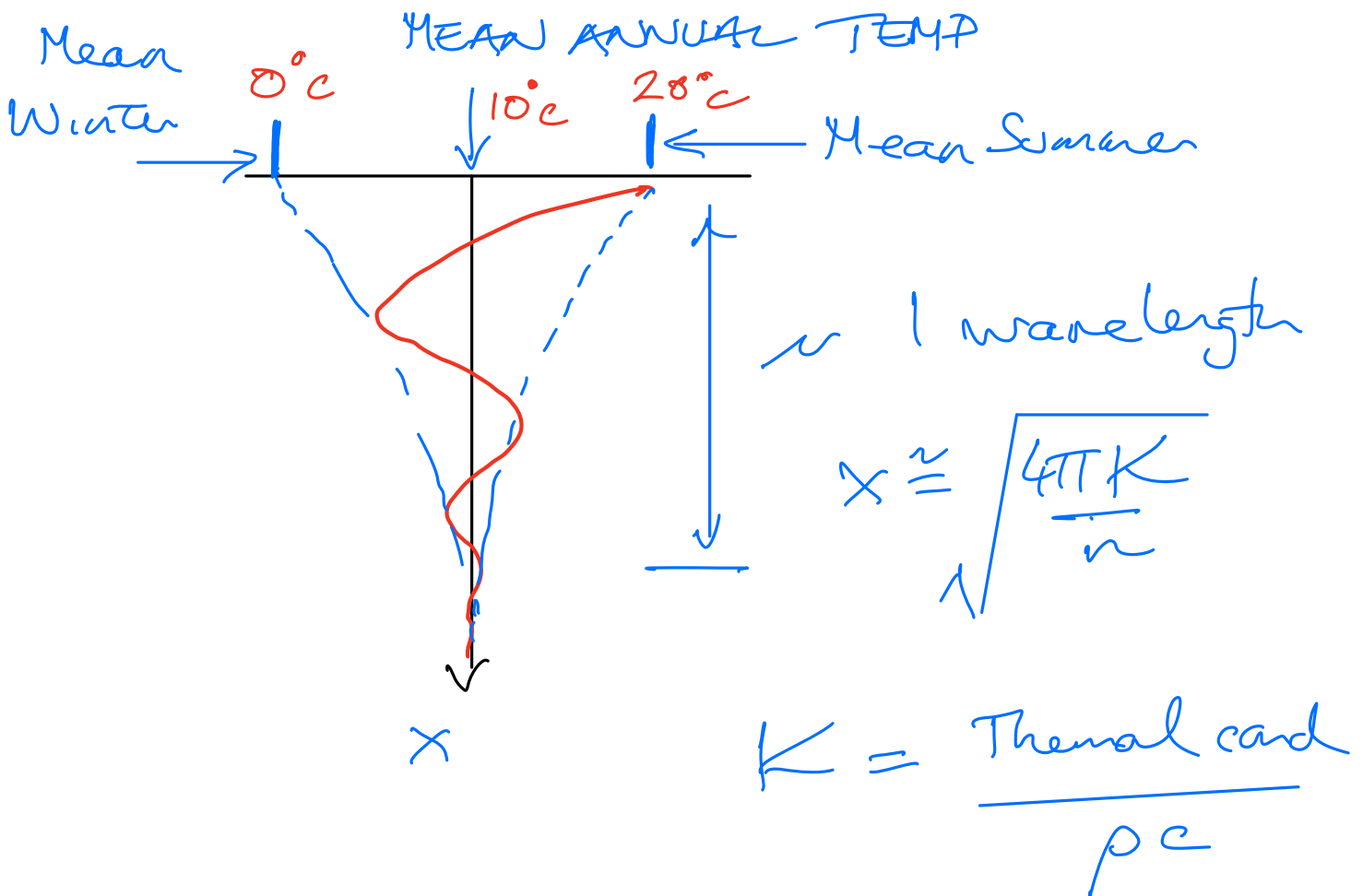
<u>Wavelength</u>	<u>Freq</u>
2.7 cm	1/min
1 m	1/day
<u>20 m</u>	1/year

$$\left(4\pi \frac{30}{1}\right)^{1/2} = \sqrt{360} \text{ m}^2/\text{yr} \cdot \text{yr}$$

$$\sim \underline{\underline{20 \text{ m}}}$$

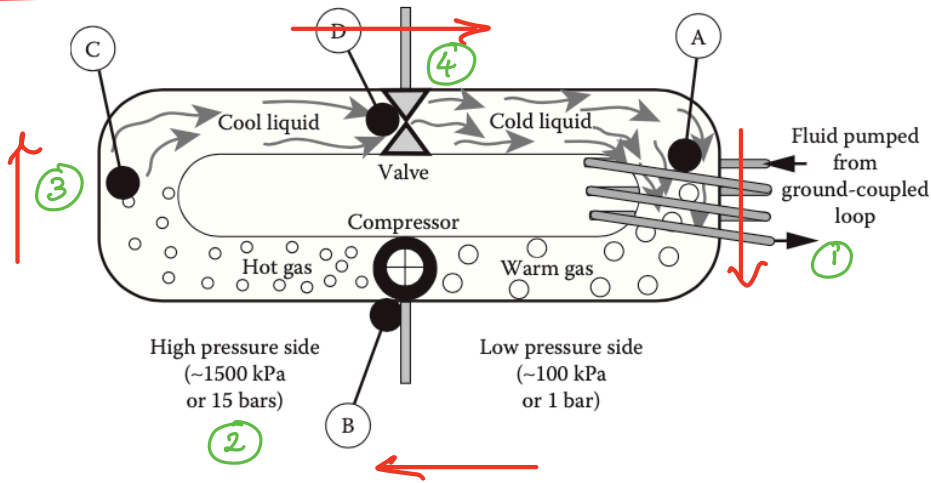


## TEMPERATURE PROFILES



2. Mechanisms of utilizing low quality heat -> high(er) quality heat?

# Thermodynamics of Heat Pumps



COIL FROM GROUND  
 $\Delta T \sim \pm 10^\circ C$

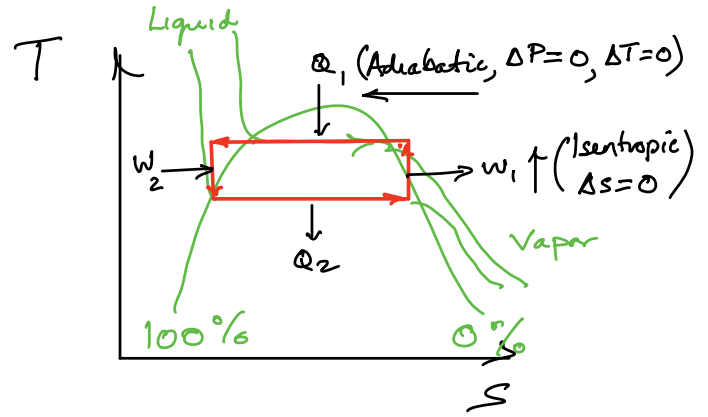
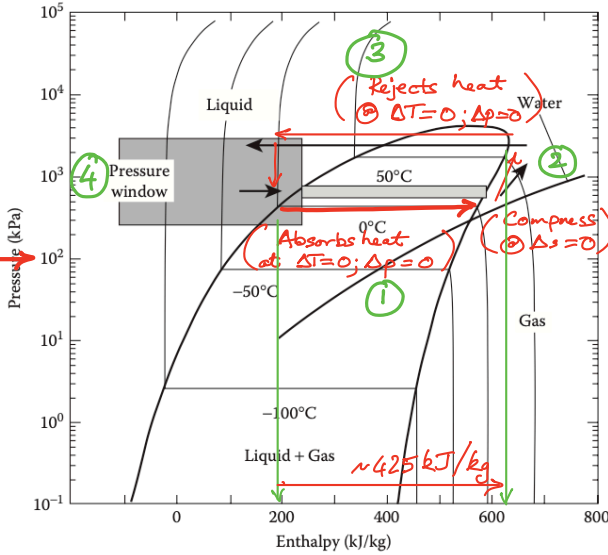


FIGURE 11.4 Enthalpy–pressure diagram for propane showing the two-phase liquid–gas region. For reference, the low-temperature limb of the liquid boundary for the water system is also shown (see Figure 3.8 for details of the water system).

CARNOT CYCLE - Same as deep geothermal.

PRINCIPLE - Heat gained leg ①  $\rightarrow$  Energy of compression in leg ②

Allows  $+\Delta H$  in leg ① (from ground - low quality)

$\rightarrow$  Rejected to building leg ③

$\rightarrow$  @ energy cost of  $\Delta p$  in ②

TUNE 2-PHASE FLUID  $\rightarrow$  0 - 50°C BP

or for PA, 0 - 20°C or  $\sim 10^\circ C$ .

i.e. Capable of liquid  $\rightarrow$  vapor @ 10°C

and  $\text{C} \text{ p} > \text{atm}$

FOR PROPANE  $\Delta H \sim 425 \text{ kJ/kg}$  (of propane)

Geothermal water  $C = 4.18 \text{ kJ/kg.K}$ .

TABLE 11.1

Thermodynamic Properties of Some Compounds Potentially Useful as Refrigerants

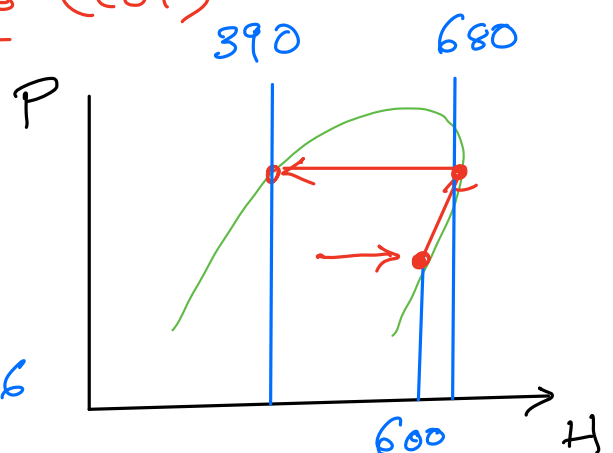
Name	Formula	Molecular Weight (g/mol)	Density (kg/m <sup>3</sup> )	Melting Temperature (°C)	Boiling Temperature (°C)	Heat of Vaporization (kJ/kg)	Constant Pressure Heat Capacity (kJ/kg-K)
R134a	H <sub>2</sub> FC-CF <sub>3</sub>	102.03	1206	-101	-26.6	215.9	0.853
Propane	C <sub>3</sub> H <sub>8</sub>	44.096	582	-187.7	<u>-42.1</u>	425.31	1.701
Isopentane	C <sub>5</sub> H <sub>12</sub>	72.15	626	-160	28	344.4	2.288

EFFICIENCY: For 1 kg of geothermal water/s and a 1.5 kW compressor

$$\frac{E_{\text{total}}}{E_{\text{consumed}}} = \frac{4180 \text{ J/s} + 0.8 \times 1500 \text{ J/s}}{1500 \text{ J/s}} \sim 3.6$$

COEFFICIENT OF PERFORMANCE (COP)

$$\text{COP} = \frac{\text{Delivered heat}}{\text{Comp. elec. demand}} = \frac{680 - 390 \text{ kJ/kg}}{680 - 600 \text{ kJ/kg}} \cong 3.6$$





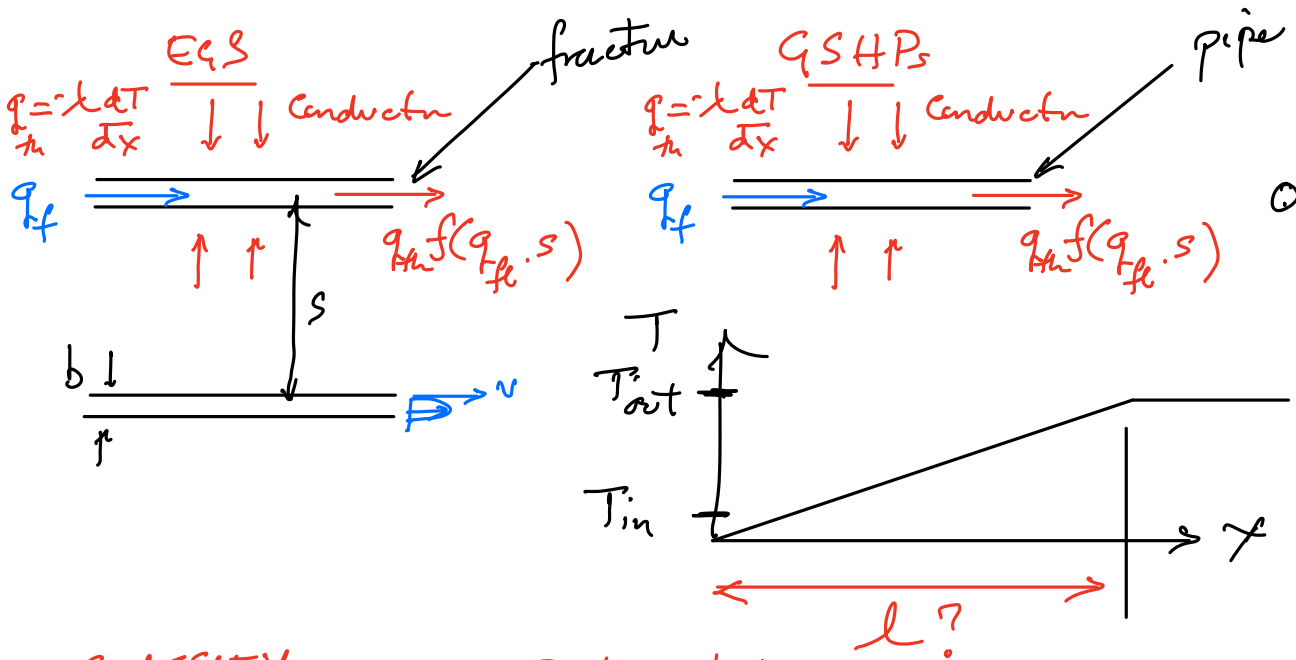
Note - assumes 100% efficiency of compressor  
(not 0.8).

# GSHPs

1. Mechanisms of heat flow in the shallow earth?
2. Mechanism of utilizing low quality heat -> high(er) quality heat?
3. Rate-limiting processes?

## HEAT FLOW IN GEOTHERMAL (WATER) SYSTEM.

Similar to EGS - Rate limited  
 - Engineered (constructed).  
 Engineered



### GLASSLEY

Heating loop:

$C_{\#} =$  Building heating load  $\sim 12$  kW (not elec load of 1 kW).

$$L_H(m) = \frac{\{(C_H) \times [(COP - 1) / COP] \times [R_P + (R_S \times F_H)]\}}{(T_L - T_{min})} \quad (11.4)$$

For a cooling loop, the corresponding equation is

$$L_C(m) = \frac{\{(C_C) \times [(EER + 3.412) / EER] \times [R_P + (R_S \times F_C)]\}}{(T_{max} - T_H)} \quad (11.5)$$

Energy Efficiency Ratio  $\equiv$  COP cooling

where:

$R_P$  is the resistance to heat flow of the pipe (which is equivalent to 1/thermal conductivity of the pipe)

$R_S$  is the resistance to heat flow of the soil (which is equivalent to 1/thermal conductivity of the soil)

$F_H$  ( $F_C$ ) is the fraction of time the heating (cooling) system will be operating

$T_L$  ( $T_H$ ) is the minimum (maximum) soil temperature at the depth of installation

$T_{min}$  ( $T_{max}$ ) is the minimum (maximum) fluid temperature for the selected heat pump

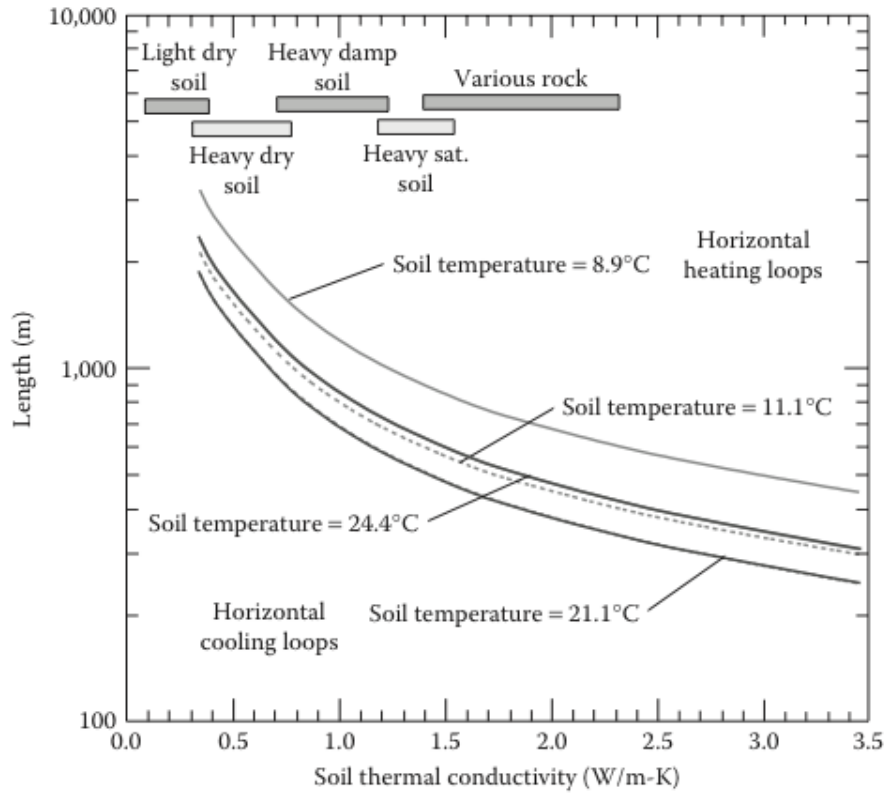
Check units:

$$\text{COP} \doteq -$$

$$T \doteq K$$

$$R \doteq 1/(W/(m \cdot K)) \doteq \frac{m \cdot K}{W}$$

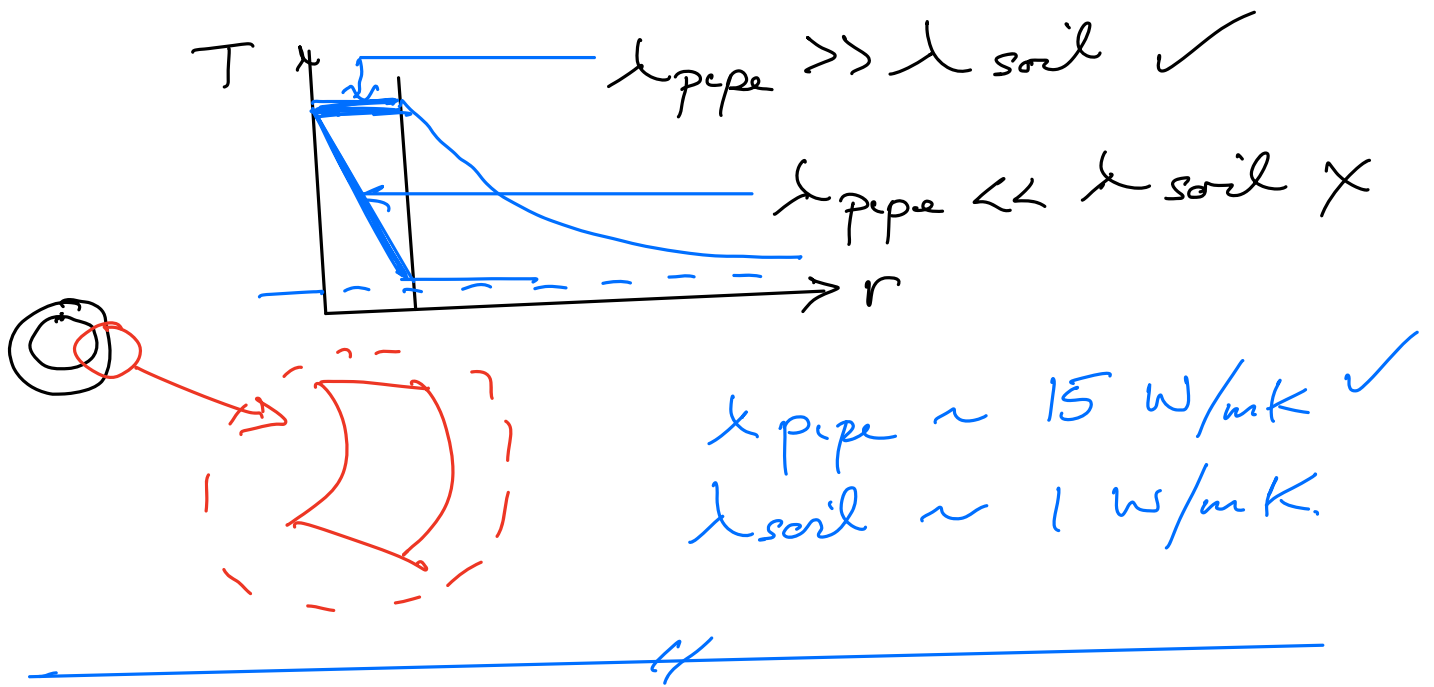
$$L_H(m) \doteq \frac{W(-) \times m \cdot K / W}{K} \doteq m \checkmark$$



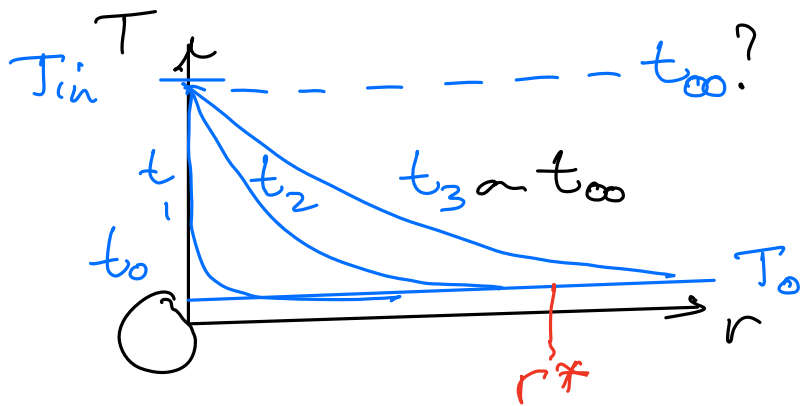
**FIGURE 11.7** Computed loop length for heating and cooling, closed-loop GHP systems. In these calculations, it was assumed that the COP of the heat pump was 3.24 and the EER was 7.8. Pipe thermal conductivity was assumed to be 14.8 W/m-K, the heating and cooling run time fractions were 0.5 and 0.6, respectively, and the heat pump fluid  $T_{\max}$  and  $T_{\min}$  were 37.8°C and 4.4°C, respectively. For reference, the range of thermal conductivities for light, dry soil (Light dry soil); heavy, dry soil (Heavy dry soil); heavy, damp soil (Heavy damp soil); heavy, saturated soil (Heavy sat. soil); and crystalline rocks (Various rock) are also shown.

Suggests a length of  $\sim 1000m$  !!

# RATIONAL BASIS FOR DESIGN

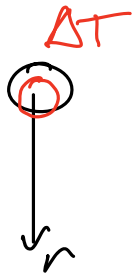
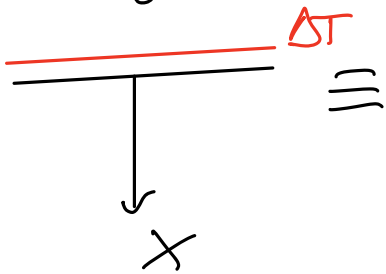


## STEADY STATE OF TRANSIENT BEHAVIOR?

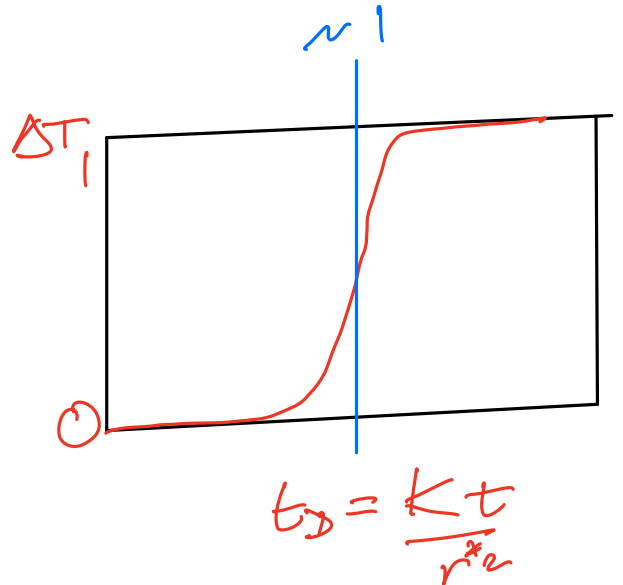


(to first order)

Analogous to:



$\Rightarrow$



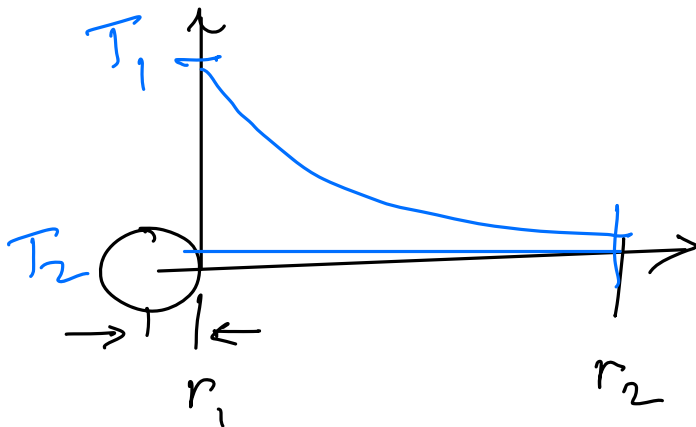
# STEADY HEAT FLOW AROUND PIPE

1. What does it look like
2. What is heat flux to pipe?
3. How long does it take (more than  $\frac{1}{2}y$ ?)

Same as water flow to well

Darcy's Law  $q = -K \frac{dh}{dr} \quad \text{or} \quad -\frac{k}{\mu} \frac{dp}{dr}$

Fourier's Law  $q = -\lambda \frac{dT}{dr}$



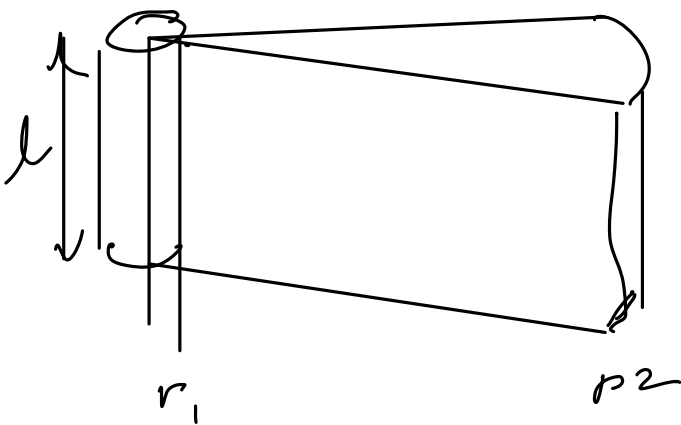
$$Q_F = 2\pi l \frac{k}{\mu} \frac{(P_2 - P_1)}{\ln(r_2/r_1)}$$

$$Q_{th} = 2\pi l \lambda \frac{(T_2 - T_1)}{\ln(r_2/r_1)}$$

This gives steady flux,

But - 1. Is steady reached?

2. If so, what is  $r_2$ ?



# IS STEADY FLUX REACHED?

$$t_D \sim 1 = \frac{kt}{r_2^2} \rightarrow r_2 \approx \sqrt{kt}$$

$\nearrow$   $1000 \text{ m}^2/\text{yr}$   
 $\searrow$   $\frac{1}{2} \text{ yr.}$

$$r_2 \sim \sqrt{16} \sim \underline{4 \text{ m}}$$

Steady flow to pipe if  $r_2 \sim 1 \text{ m}$

$$r_1 \sim 1 \text{ cm} = 10^{-2} \text{ m}$$

Thermal load for house?  $\sim 10 \text{ kW}$   
(not  $1 \text{ kW}$  for elec)

$$\underline{Q = 10^4 \text{ W}}$$

Soil conductivity  $\sim k = 1 \text{ W/(m.K)}$

Temperature drop  $\sim 10^\circ \text{C} = \Delta T$

$$\ln(4/10^{-2}) \sim 6.0$$

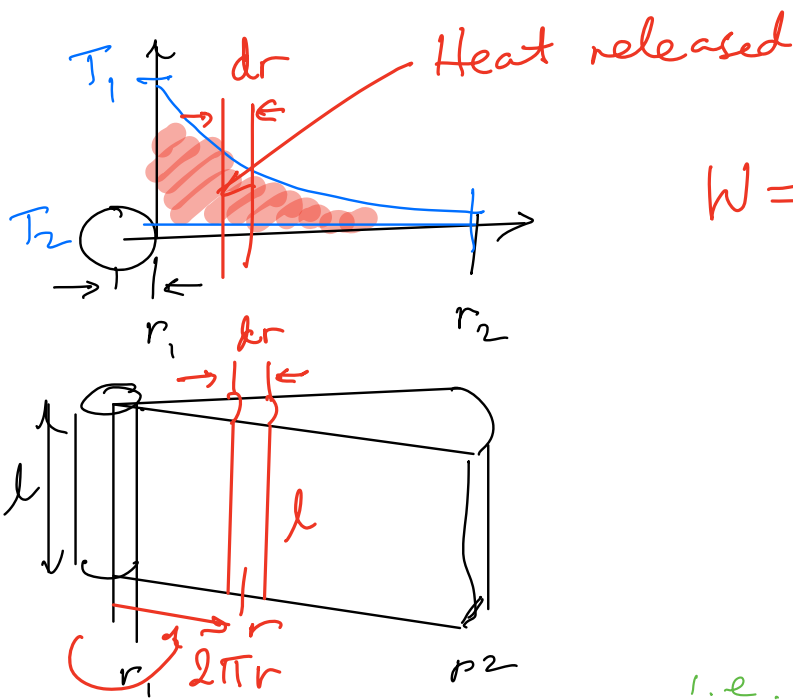
$$Q_m = 2\pi l k \frac{(T_2 - T_1)}{\ln(r_2/r_1)}$$

$$l = \frac{Q \ln(r_2/r_1)}{2\pi \cdot k \cdot \Delta T}$$

$$l = \frac{10^4 \text{ W} \cdot 6}{2\pi \cdot 1 \text{ W/(mK)} \cdot 10 \text{ K}}$$

$$l \sim 10^3 \text{ m QED.}$$

How MUCH HEAT RELEASED FROM STORAGE  
IN GETTING TO STEADY STATE?



$$W = \rho c T$$

$$W = \int \frac{2\pi r dr l}{\cancel{\rho}} \rho c T$$

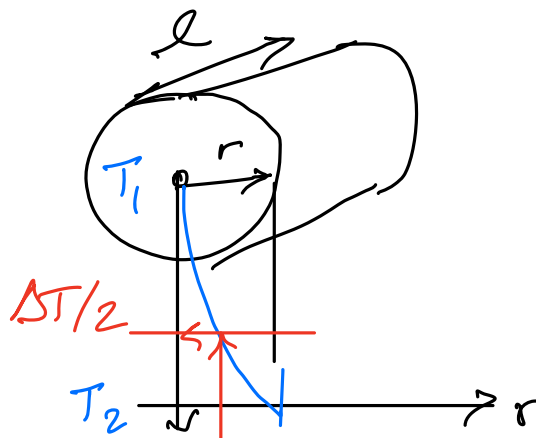
recover for  $T = f(r)$

i.e. set  $Q = \text{known}$

for  $(r_1/r_2)$  then

determine  $r_3$ .

Estimate:



1000 m

10°C/2

$$W = V \rho c T = \pi r^2 \cdot l \cdot \rho c \cdot T$$

$4m$ 
 $2000kg/m^3$ 
 $1000J/kg \cdot K$

$$W = (50m^2)(1000m)(2000kg/m^3) \times (1000J/kg \cdot K) \times 5^\circ C$$

$$W = 10^2 10^3 10^3 10^3 \times 5 = 5 \times 10^{11} J \text{ in } \frac{1}{2}y$$

$$= \underline{5 \times 10^{11} J \text{ in } \frac{1}{2}y}$$

$$\frac{1}{2}y = 10^5 s \times 100d \approx 10^7 s$$

$$\text{Power is } \frac{W}{t} = \frac{5 \times 10^{11} J}{10^7 s} \approx 5 \times 10^4 \frac{J}{s}$$

$$\text{Power from storage} = 50kW$$

$$\text{Power for steady state} = \underline{10kW}$$

Assumed house load for  
Steady state

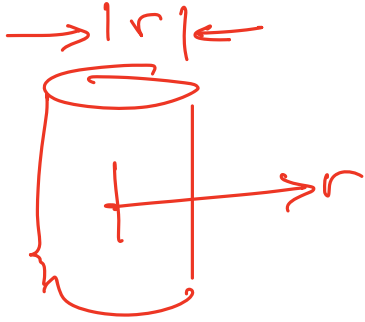
Conclusion: Radius of cooling in soil less than 4m. since storage supplies  $\times 5$  of steady for

QED



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How long to cool a can of seltzer or  
cook a steak?



$$t_D = \frac{Kt}{r^2} \sim 1$$

$$K = \frac{\lambda}{\rho c} \sim \frac{0.5 \text{ W/(m}\cdot\text{K)}}{10^3 \text{ kg/m}^3 \cdot 4.1 \text{ kJ/kg}\cdot\text{K}}$$

$$K \sim 0.1 \times 10^{-6} \text{ m}^2/\text{s}$$

$$t \sim (r^2/K) \sim (2 \times 10^{-2} \text{ m})^2 / 0.1 \times 10^{-6}$$

$$\sim \frac{4 \times 10^{-4}}{0.1 \times 10^{-6}} \sim 40 \times 10^2 \text{ s}$$

$$\underline{4000 \text{ s} \sim 60 \text{ min} \sim 1 \text{ hr.}}$$

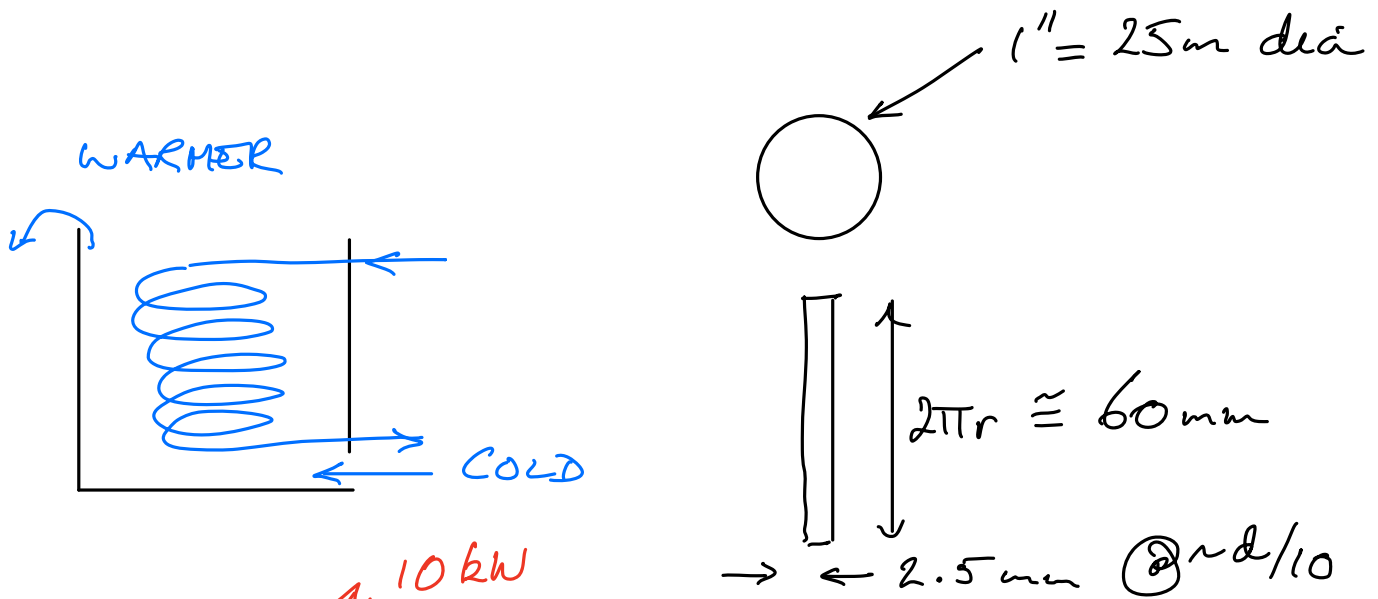
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Note scaling with  $r^2$

Cooking a steak. Double the thickness

Quadruple to cooking time

# USE OF B/H HEAT EXCHANGER OR CRYPT



$$Q = A k \frac{dT}{dx} = \frac{L \times (60 \times 10^{-3} \text{ m}) \times 1 \cdot 10}{2.5 \times 10^{-3} \text{ m}}$$

$$\frac{10^4 \cdot (2.5 \times 10^{-3} \text{ m})}{(60 \times 10^{-3} \text{ m}) \times 1 \times 10} = \frac{\text{N} \cdot \text{m}}{\text{s}} \frac{\text{m} \cdot \text{K} \cdot \text{m}}{\text{m} \cdot \text{N} \cdot \text{m} / \text{s} \cdot \text{K}}$$

$$L \approx 10^4 \left( \frac{2.5}{60} \right) \frac{1}{10} \sim 1/20$$

$$L \sim \frac{10^3}{20} \sim 50 \text{ m} \quad \text{Q.E.D.}$$

Volume of water needed to maintain temp

$$10 \text{ kW} = 10^4 \text{ W} = \dot{m} c \Delta T$$

$$\dot{m} \sim 10^4 \text{ J/s} / (c \Delta T) \sim 10^4 / (4.1 \times 10^3) \cdot 10$$

$$\dot{M} \sim 0.25 \text{ kg/s}$$

$$10^5 \text{ secs} = 0.25 \times 10^5 \text{ kg} = 25 \times 10^3 \text{ kg/d.}$$