Bromine, nitric acid, and palladium dichloride react, at sufficiently high vapor pressures, with graphite to form second-stage  $C_{16}Br_2$  (<sup>1</sup>), second-stage  $C_{48}$  +NO<sub>3</sub> - 3HNO<sub>3</sub> (<sup>3</sup>) and third-stage  $C_{10,7}$  PdCl<sub>2</sub> (<sup>3</sup>). Kinetics of bromination of graphite have been studied in some detail  $(4^{-3})$ , but rates of intercalation of HNO<sub>3</sub> and PdCl<sub>2</sub> have not yet been studied from the same kinetic point of view. Comparative studies of rates of intercalation might be expected to clarify mechanisms of intercalation and to permit useful generalizations. Nitric acid, palladium chloride, and bromine were chosen for study because they intercalate respectively as a two-dimensional liquid-like layer (8), a disordered two-dimensional solid, and an ordered solid(1). Higher-stage intercalates of bromine and nitric acid are also known, and it is of interest to know whether changes in rate of diffusion attribute to the formation of discrete stages can be observed.

Cylindrical wafers of stress-annealed, highly oriented pyrolytic graphite used in these experiments have mosaic spreads (FWHM)  $\leq 2$  deg. Weight gains of graphite wafers suspended in HNO<sub>3</sub> and Br<sub>2</sub> vapors are monitored continuously by a recording microbalance, and rates of weight gain in HNO<sub>3</sub> vapor are monitored using a derivative computer. Temperature of the wafer is maintained  $\sim 3$  deg higher than that of the intercalant reservoir by which the vapor pressure of intercalant is fixed. Graphite wafers are exposed to PdCl<sub>2</sub> vapor by packing them in PdCl<sub>2</sub> powder in a quartz boat and heating in flowing Cl<sub>2</sub>.

Weight gains  $M_t$  at time, t, during intercalation are plotted as fractions of the ultimate weight gain  $M_{\infty}$ corresponding to formation of the lowest-stage compound for Br<sub>2</sub> and PdCl<sub>2</sub> in Figure 1 and for HNO<sub>3</sub> in Figure 2. Figure 1 shows an initial "induction period" during which little weight gain occurs, and a region in which  $M_t/M_{\infty}$ increases linearly with  $t^{\frac{1}{2}}$  as expected for a diffusion process. The "induction period" region has been omitted for clarity's sake from Figure 2, which shows a third region, during which  $M_t/M_{\infty}$  increases more slowly with time than in the second region. Diffusion coefficients, D, calculated from the expression<sup>5</sup>

where r is the radius of the wafer, are shown in Table I. Rates of intercalation increase linearly with  $t^{-\frac{1}{2}}$  when the contribution of  $t^{\frac{1}{2}}$  is small, as expected from the time derivative of Equation 1 and as shown in Figure 3 for a typical bromination reaction. Nitration can thus be attributed to a process characterized by a single diffusion coefficient up to  $M_t/M_{\infty} = 0.50$ , a weight gain corresponding to formation of Stage III graphite nitrate, and bromination can be characterized by a single diffusion coefficient at least up to  $M_t/M_{\infty} = 0.25$ . X-ray diffraction scans of graphite wafers exposed to PdCl<sub>2</sub> vapor until  $M_t/M_{\infty} \approx 0.5$  and then quenched show only the (002) reflections of Stage III  $C_{18}$ , PdCl<sub>2</sub>. No higher-stage compound is observed; indeed, none is known. Electron microprobe analysis of the cleavage surface of such a wafer yields the plot of Cl<sub>2</sub> intensity versus radial distance shown in Figure 4. The pronounced reaction front and absence of lower-stage compounds shown here, and the linearity of  $M_t/M_{\infty}$  shown in Figure 1, are expected for a process characterized by a single diffusion coefficient.

The diffusion coefficient of HNO<sub>3</sub> in graphite at 30°C increases with increasing HNO<sub>3</sub> vapor pressure as shown in Table I, and seems in fact to be proportional to vapor pressure. The diffusion coefficient of PdCl<sub>2</sub> increases with increasing vapor pressure of PdCl<sub>2</sub> and with increasing temperature. Values of log  $D_{PdCl_2}$  fall closely on a straight line when plotted versus 1/T. The activation energy for diffusion calculated from the slope of this line is approximately 35 kcal/mole. For comparison, the activation energy for diffusion of Br<sub>2</sub> in graphite is approximately 6 kcal/mole. (<sup>7</sup>)

## References

1. T. Sasa, Y. Takahashi and T. Mukaibo, Carbon <u>9</u>, 407 (1971).

2. A. R. Ubbelohde, Proc. Roy. Soc. (London) <u>A304</u>, 25 (1968).

3. Yu. N. Novikov, V. A. Postnikov, Ya. V. Salyn, V. I. Nefedov and M. E. Volpin, Izv. Akad. Nauk. SSSR, Ser. Khim (1973) 1689. [Bull. Acad. Sci. SSSR, Ser. Chem. (1973) 1653.]

- 4. J. G. Hooley, Canadian J. Chem. 40, 749 (1962).
- 5. J. G. Hooley and J. L. Smee, Carbon 2, 135 (1964).
- 6. J. G. Hooley, W. P. Garby and J. Valentin, Carbon
- <u>3</u>, 7 (1965).

7. T. Mukaibo and Y. Takahashi, Bull. Chem. Soc. Japan <u>36</u>, 625 (1963).

8. D. E. Dixon, G. S. Parry, and A. R. Ubbelohde, Proc. Roy Soc. 291A, 324 (1966).

Table I						
Diffusion	of	Intercalants	into	Highly-Oriented		

Pyrolytic Graphite						
Intercalant	Vapor Pressure, Torr	Intercalation Temperature °C	D, cm <sup>2</sup> /min.			
Brz	258	30	$1.47 \times 10^{-6}$			
HNO3	81 81 37	30 40 30	$203 \times 10^{-6}$ 133 x 10^{-6} 85 x 10^{-6}			
PdCl <sub>2</sub>	2. $10 \times 10^{-4}$ 1. $04 \times 10^{-3}$ 8. $82 \times 10^{-3}$	416 450 500	0. $16 \times 10^{-6}$ 0. $52 \times 10^{-6}$ 2. $46 \times 10^{-6}$			



Figure 1. Increases of  $Br_2$  and  $PdCl_2$  with  $t^{\frac{1}{2}}$ .



Figure 2. Increases of  $HNO_3$  with  $t^{\frac{1}{2}}$ .



Figure 3. Rate of bromination at 30°C as a function of  $t^{\frac{1}{2}}$ .



Figure 4. Chlorine concentration of a graphite wafer exposed to PdCl<sub>2</sub> until  $M_t/M_{\infty} \approx 0.50$  then quenched, as a function of fractional distance  $r/r_0$  from the center of the wafer.