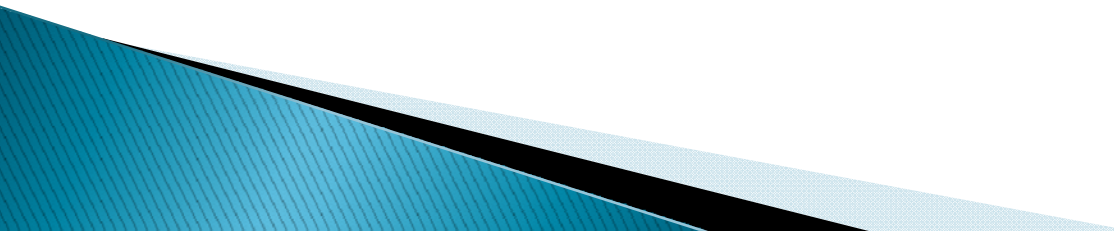


# **CO<sub>2</sub> Capture, Utilization and Sequestration**

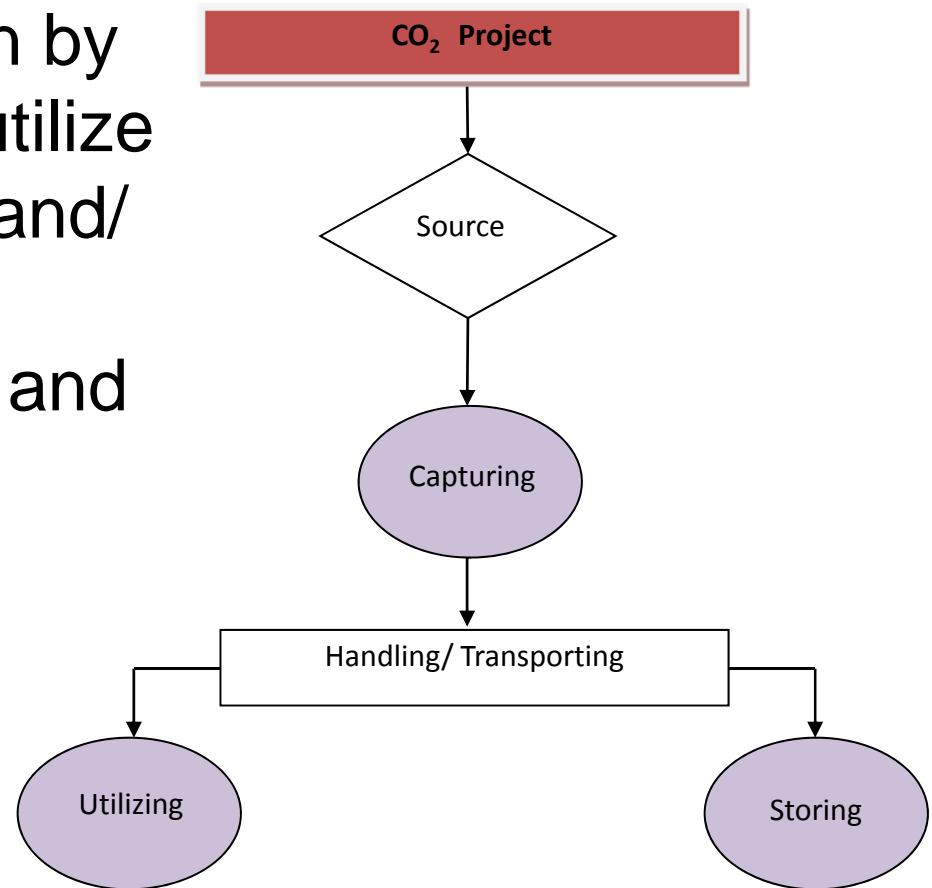
Bander Al Ghamdi  
Kyungsoo Kim  
Seyhan Emre Gorucu  
Yogesh Bansal

# Outline

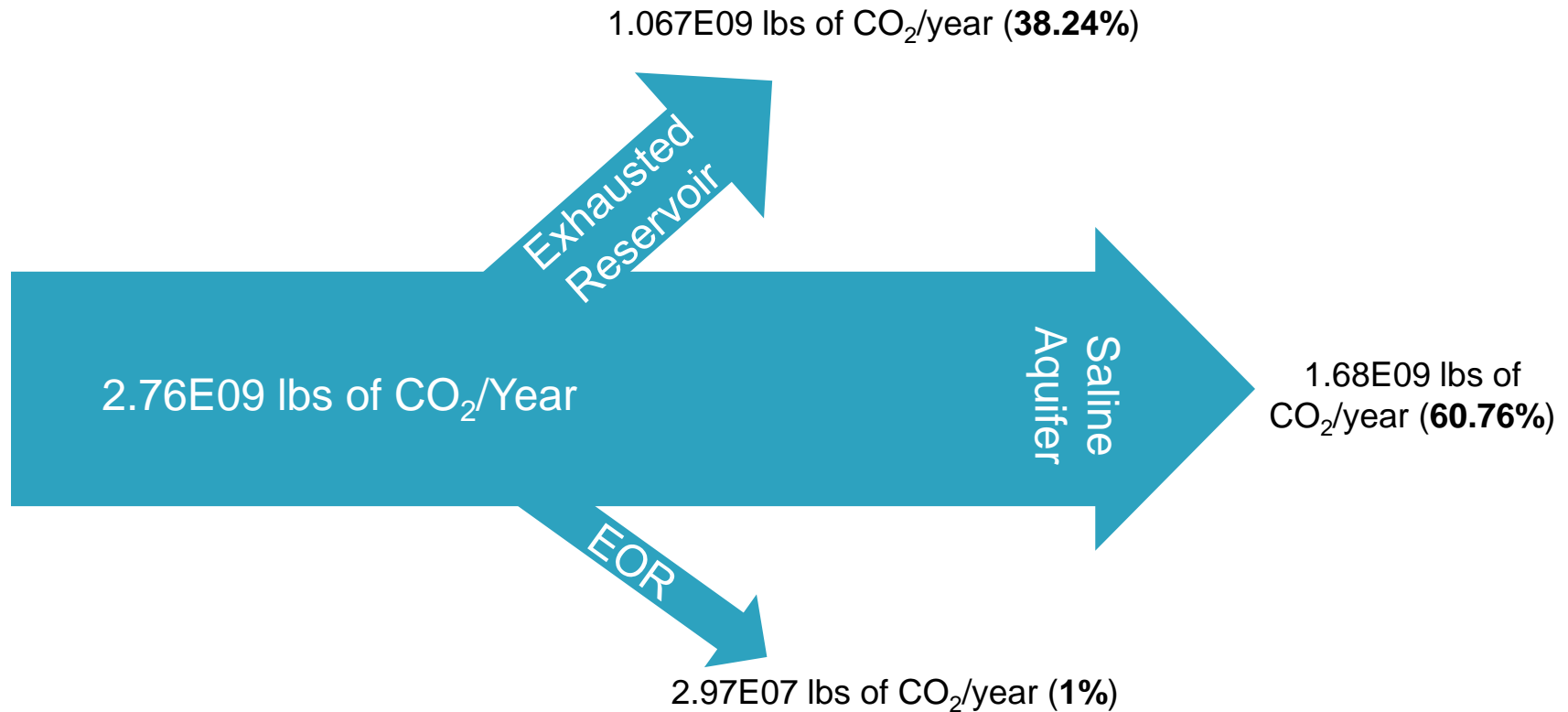
- ▶ Team Statement
  - ▶ Results
  - ▶ Approach
    - Capturing
    - Sequestration
    - Utilization
  - ▶ Conclusion
- 

# Team Statement

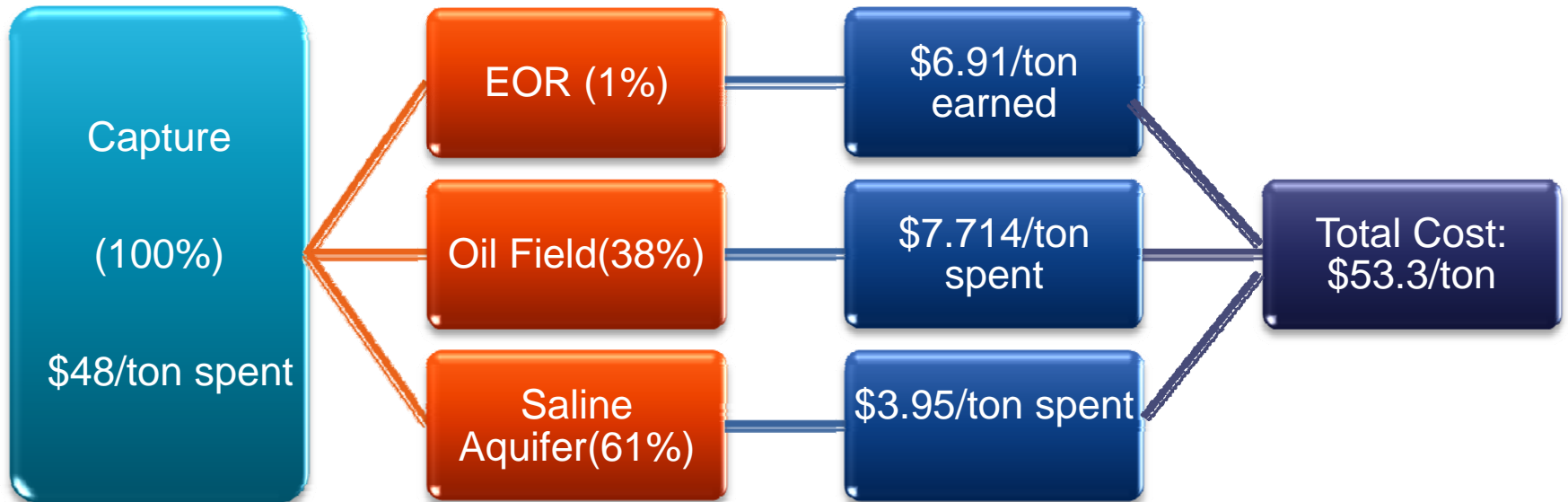
- ▶ Reduce CO<sub>2</sub> emission by efficiently capture it, utilize it for EOR purposes, and/or sequester it, while considering technical and economical analysis.



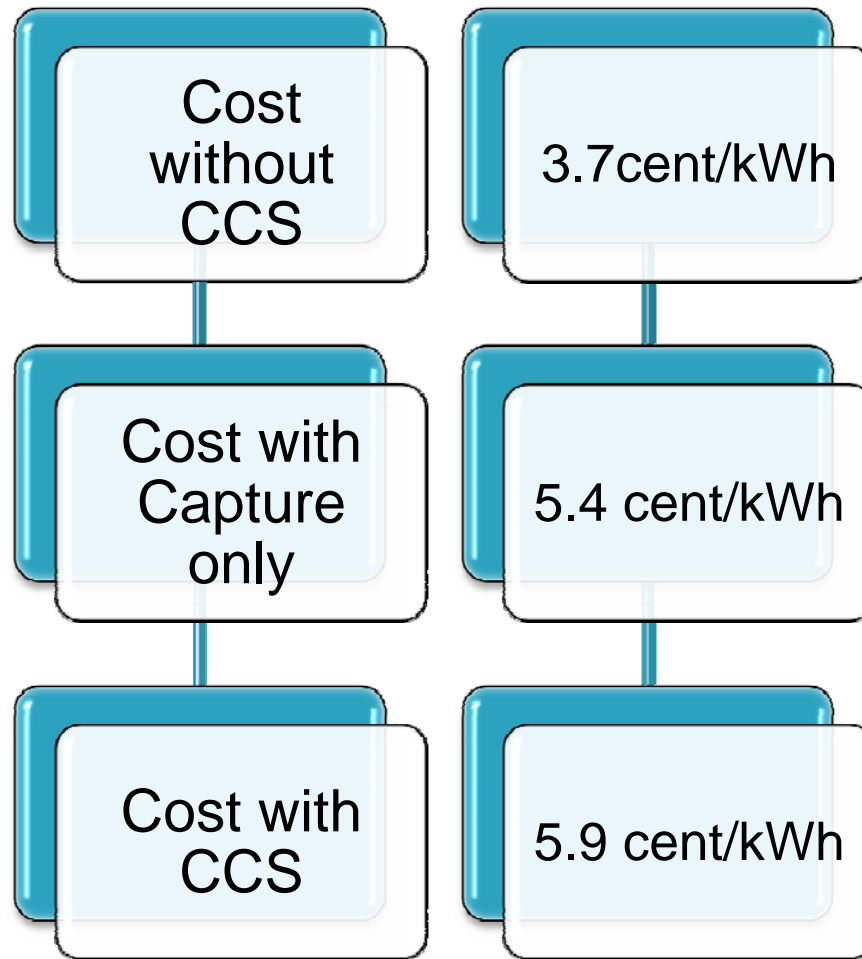
# Capture, Sequestration, and Utilization



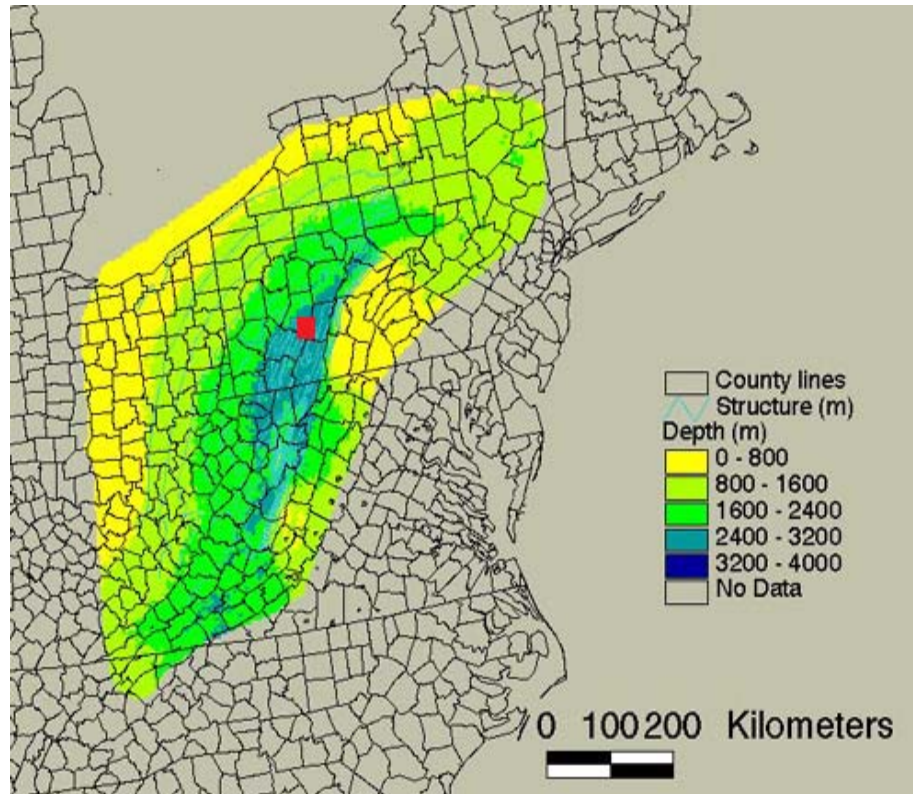
# Economical Balance



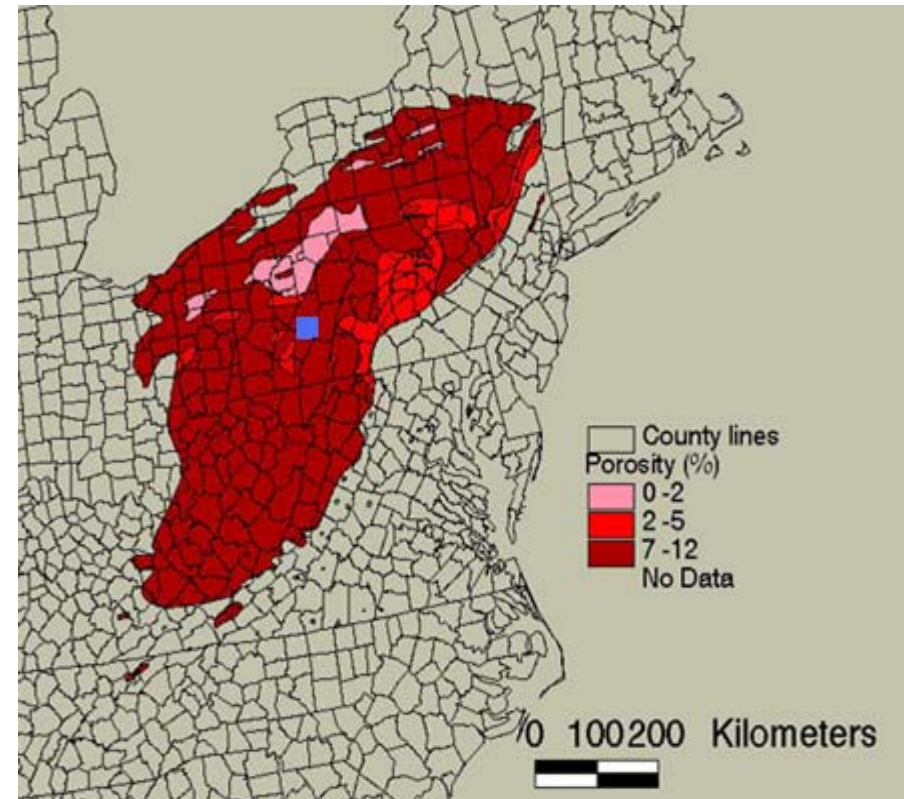
# Electricity Production Cost



# Oriskany Saline Aquifer, Seward, Pennsylvania



Depth Map

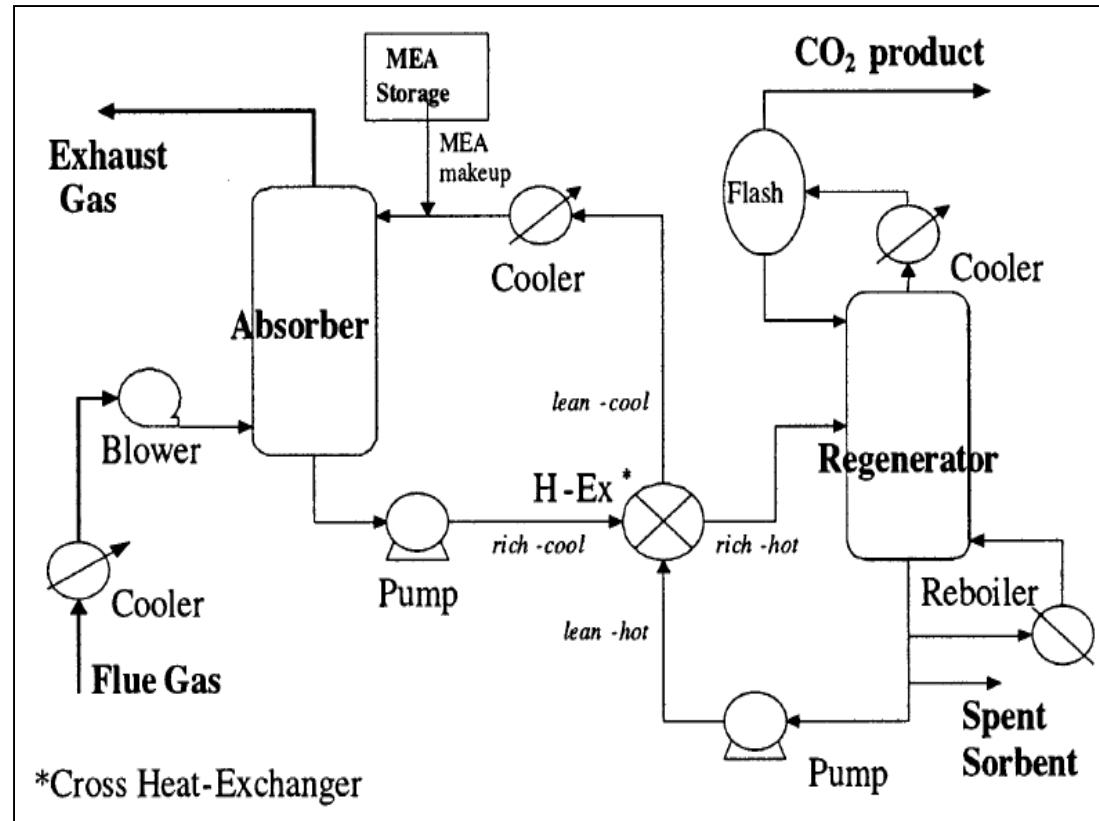


Porosity Map

# CO<sub>2</sub> capture

## ▶ Capture method

- Post-combustion
  - Chemical absorption
  - Membrane
- Pre-combustion
- Oxy-fuel



Data Source :

Rao A, Rubin E, A technical, economic, and environmental assessment of Amine-based CO<sub>2</sub> capture technology for power plant greenhouse gas control in Environ1



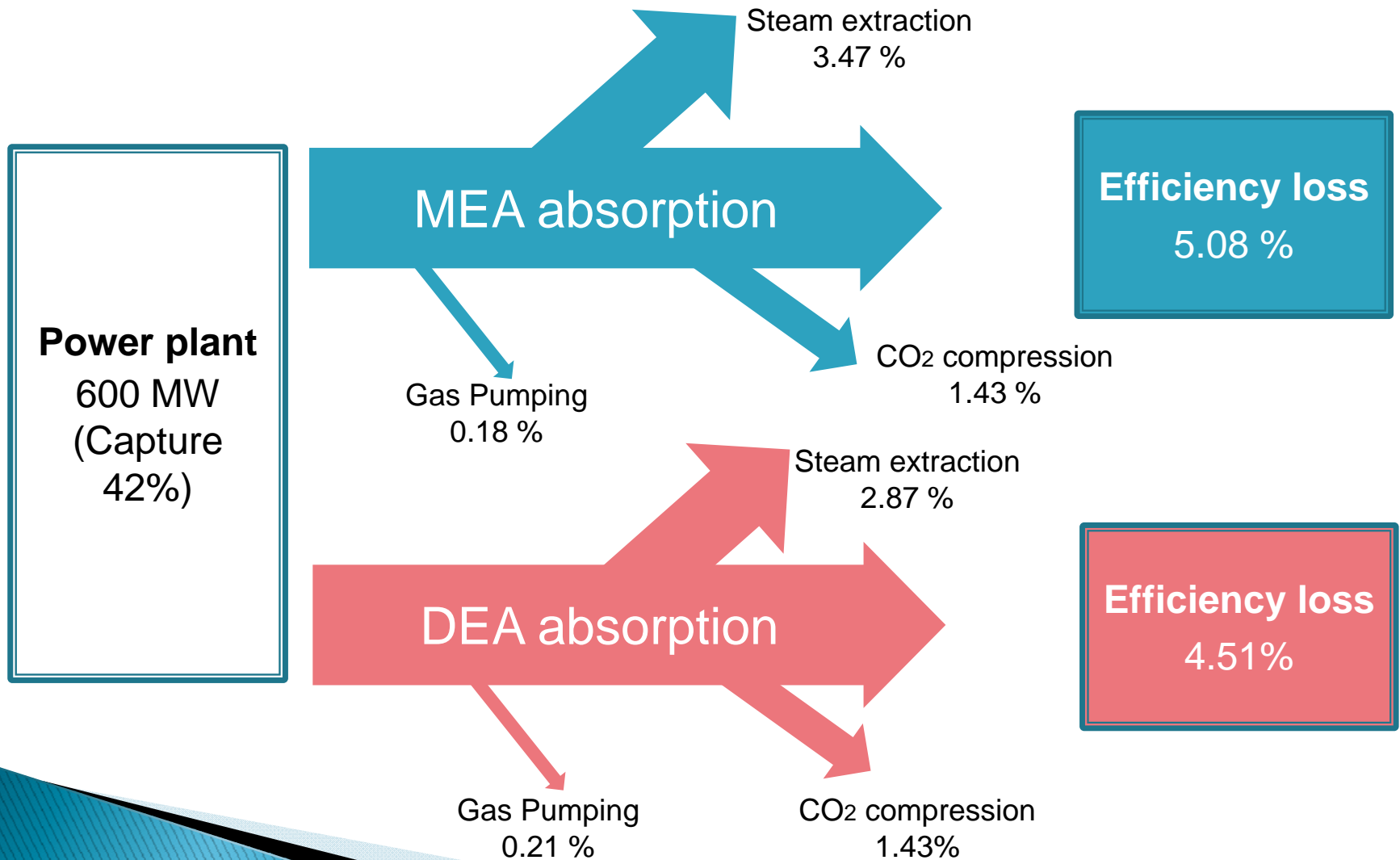
# Assumptions

- ▶ Reduce 1% of PA's annual CO<sub>2</sub> emission from the power industry and keep the emission amount the same for ten years
- ▶ Values for power plant efficiency and capital cost are the same as those of similar power plants
- ▶ No capital cost for power plant, the capital cost for power plant starts to be paid from the first running point of the capture process

## <Economic analysis assumptions>

Project life (years)	10
Operating hours (hour/year)	6000
Operation and maintenance cost (% of capital cost)	3
Spent solvent making up (\$/ton CO <sub>2</sub> captured)	4
Interest rate (%)	5
Coal price (\$/ton)	48
SO <sub>2</sub> , NO <sub>x</sub> in flue gas (ppm)	70

# Energy balance

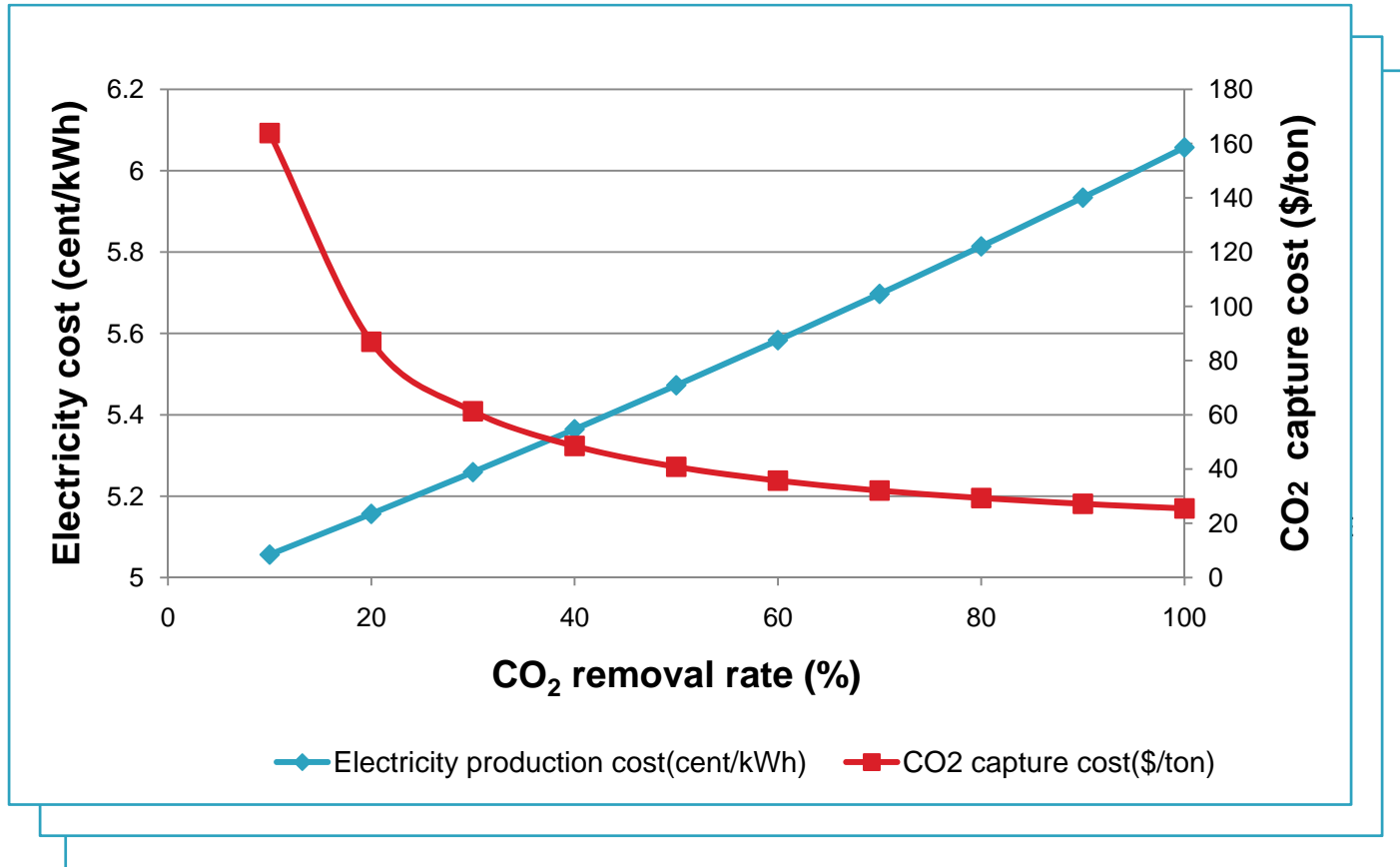


# Economical analysis

## ▶ CO<sub>2</sub> capture with MEA

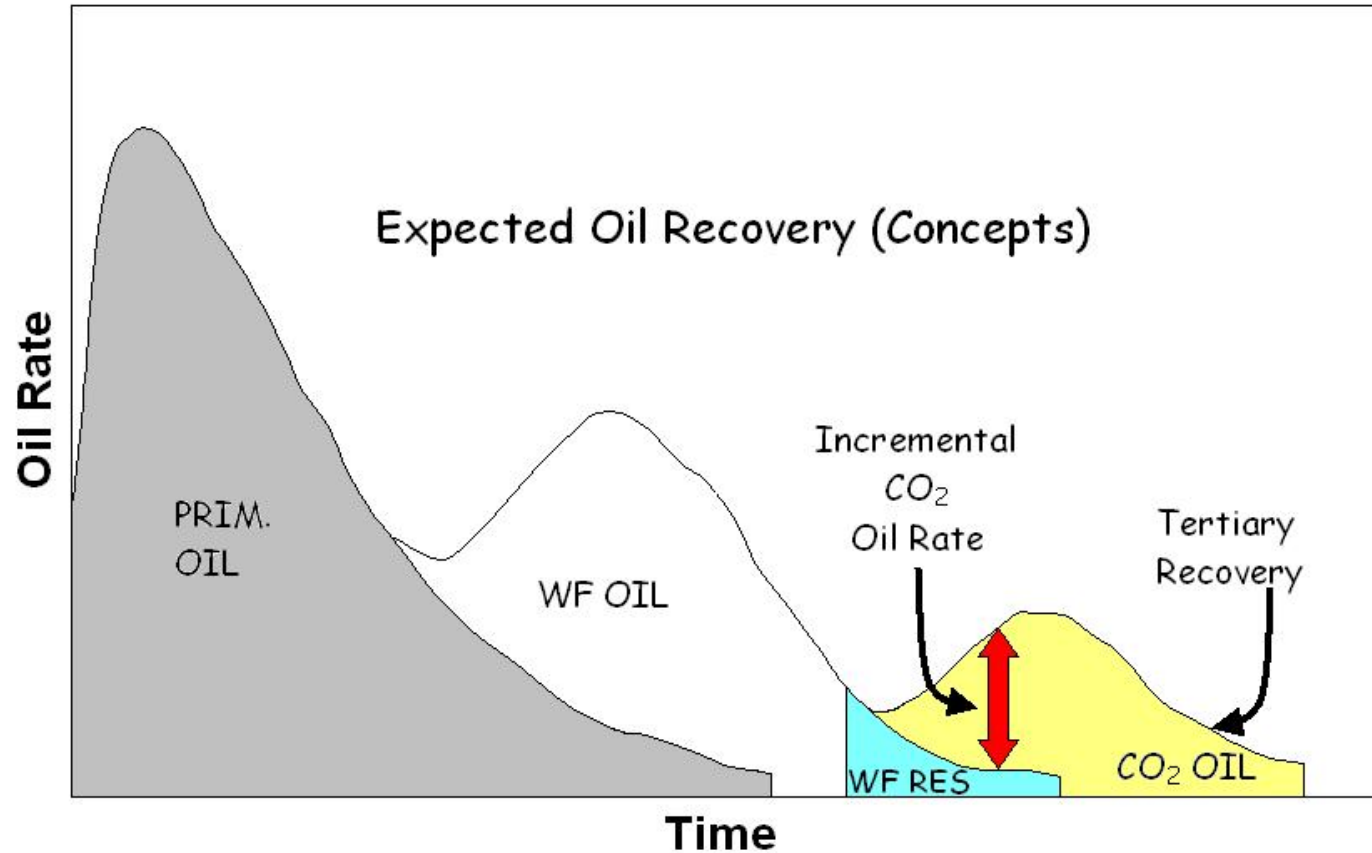
Capital cost(million USD)	957	Net power production(MW)	
Reference plant Construction	690	Reference plant	600
Chemical absorption unit	182	Power plant with CO <sub>2</sub> capture	568
CO <sub>2</sub> compressor	25		
Interest during construction and land site	59	Specific CO <sub>2</sub> emission (lb/kWh)	
		Reference plant	1.8
Annualized cost(million USD/year)	162	Power plant with CO <sub>2</sub> capture	1.1
Capital charges for reference plant	49	<b>Electricity production cost(cent/kWh)</b>	
Capital charges for CO <sub>2</sub> capture components	19	Reference plant	<b>3.7</b>
Coal feedstock	63	Power plant with CO <sub>2</sub> capture	<b>5.4</b>
Operation and maintenance cost for reference plant	22	<b>CO<sub>2</sub> capture cost (\$/ton CO<sub>2</sub>)</b>	
Operation and maintenance cost for CO <sub>2</sub> capture process	9		<b>48.6</b>

# Further analysis



# CO<sub>2</sub> for EOR

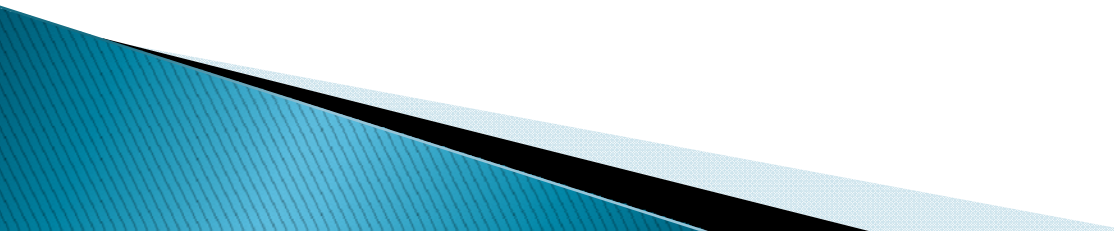
## Oil Recovery Volumes



Data Source:

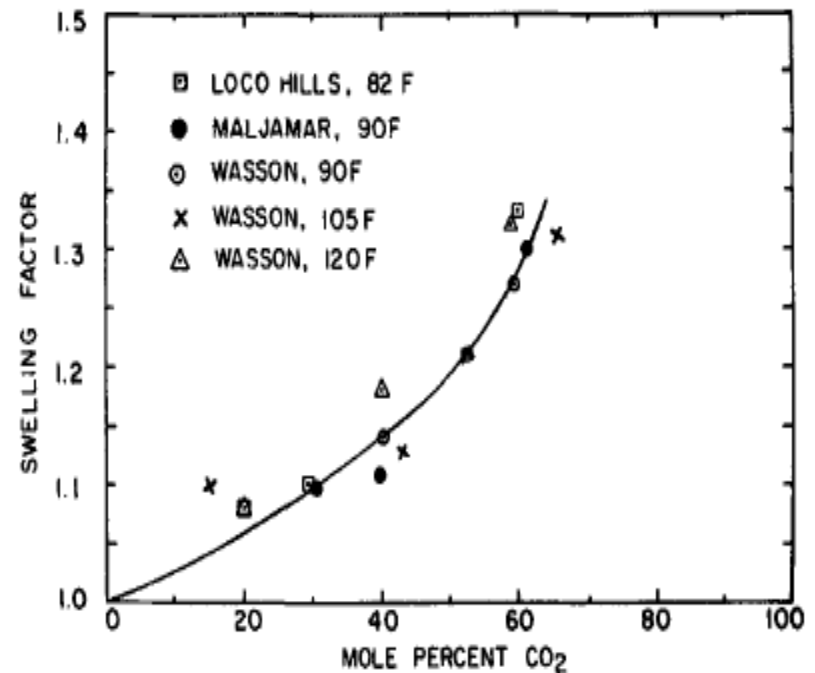
1. [www.apegga.org/Members/Presentations/Baker.ppt](http://www.apegga.org/Members/Presentations/Baker.ppt)

# Why EOR?

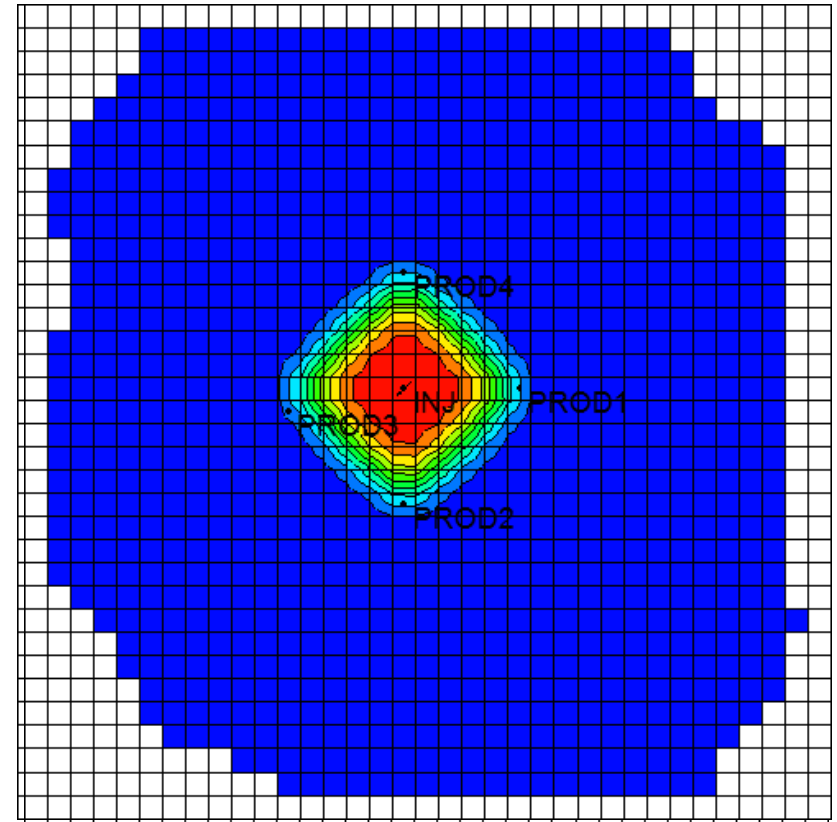
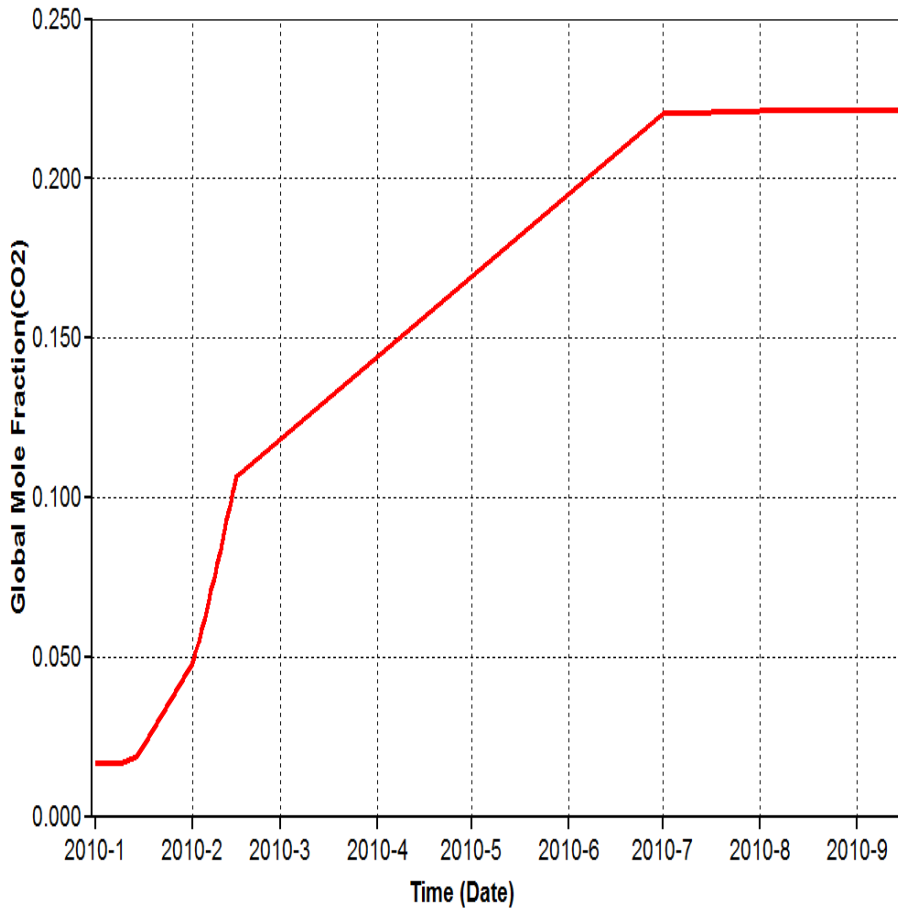
- ▶ Field production is a strong function of (P and T)
    - Lithology of the reservoir
    - Properties of oil
  - ▶ Oil could be at a high viscosity that prevents it from flowing, or it could be strongly attached to the grains inside the pore spaces where it is unreachable.
  - ▶ A mechanism has to take place to make oil more soluble and be pushed to the production zones.
- 

# Swelling vs. Concentration

- ▶ As the  $\text{CO}_2$  comes in contact with oil, it dissolves in the droplets of oil and occupies some volume allowing the oil to swell
- ▶ Oil droplets will merge together to unite in one body of fluid flow more easier to reach the production zones



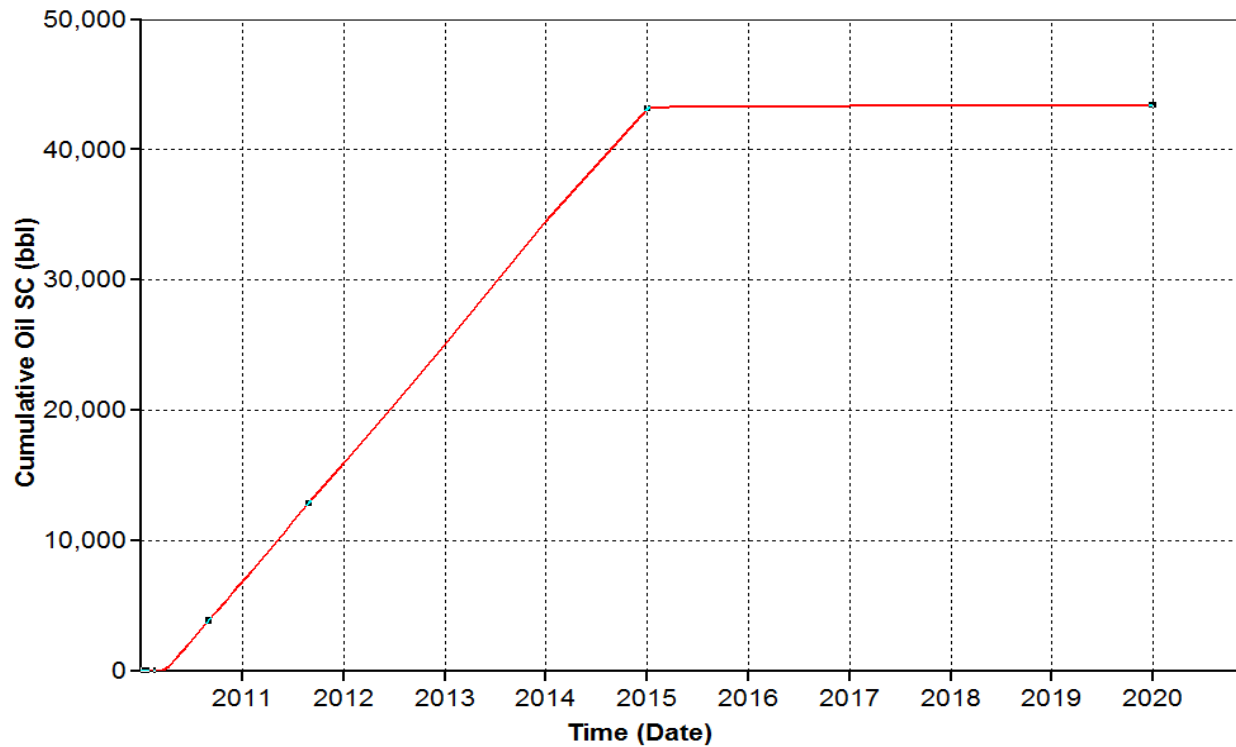
# Displacement of CO<sub>2</sub>



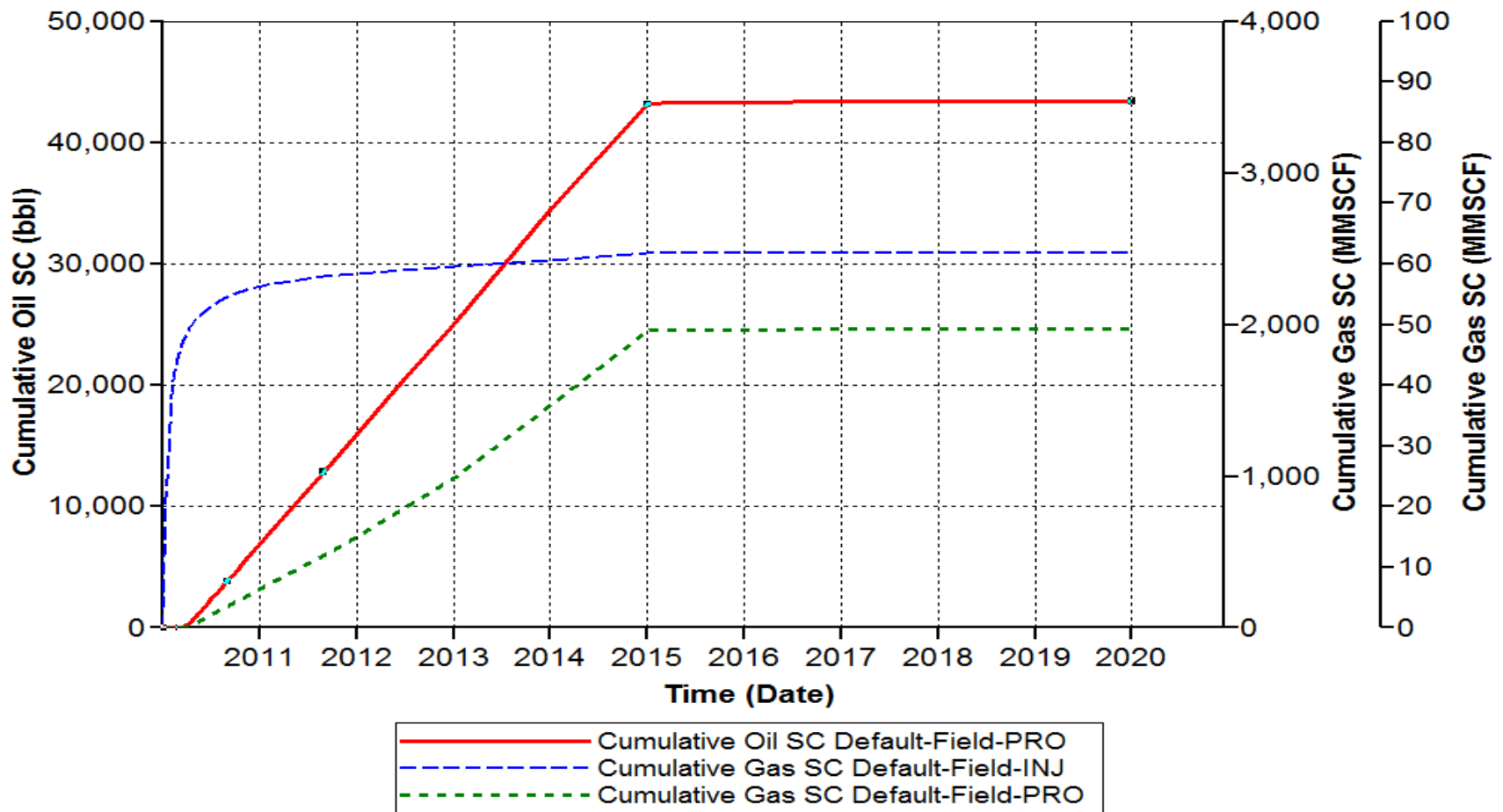


# Production Scenario

Injection Rate (MMSCF/D)	Cum. Oil Produced (MSTB)	Recovery Factor (%)
70	43	35.8



# Cycling CO<sub>2</sub>



# Exhausted oil/gas reservoir

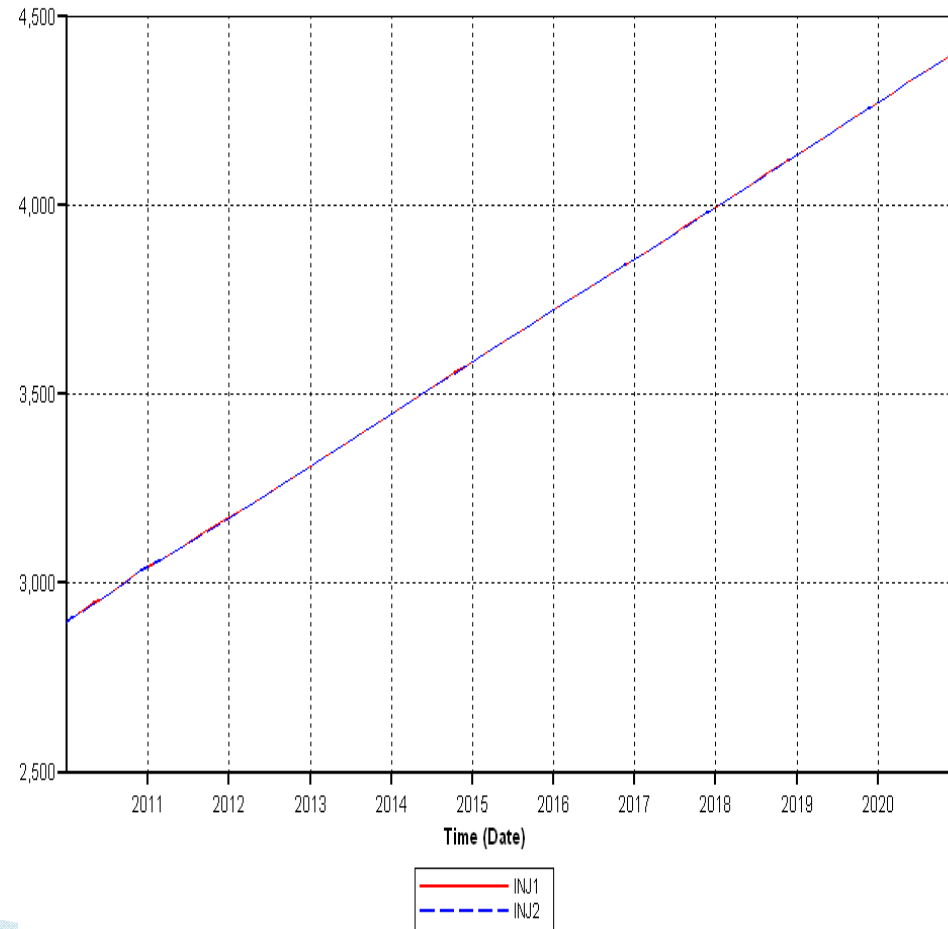
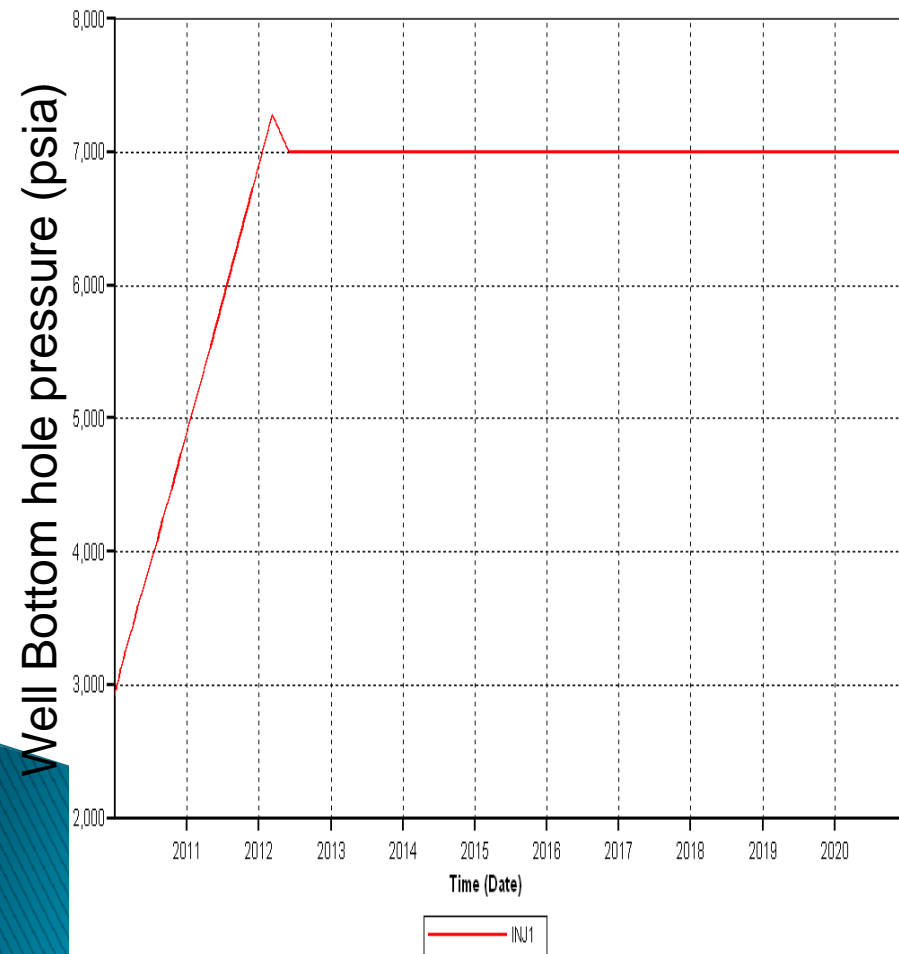
## Pore volume calculations

Layer	# of Active reservoir blocks	$\Delta x$	$\Delta y$	h	$\phi$	Pore Volume (ft <sup>3</sup> )
1	972	300	300	16	0.1373	1.922*10 <sup>8</sup>
3	972	300	300	12	0.1622	1.703*10 <sup>8</sup>
5	972	300	300	6	0.075	0.394*10 <sup>8</sup>
7	972	300	300	6	0.075	0.394*10 <sup>8</sup>
					Total	4.413*10 <sup>8</sup> ft <sup>3</sup>

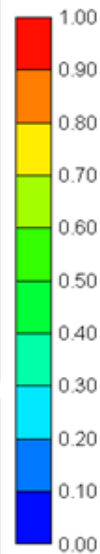
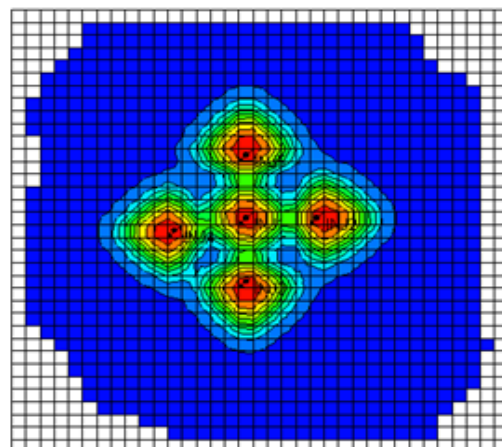
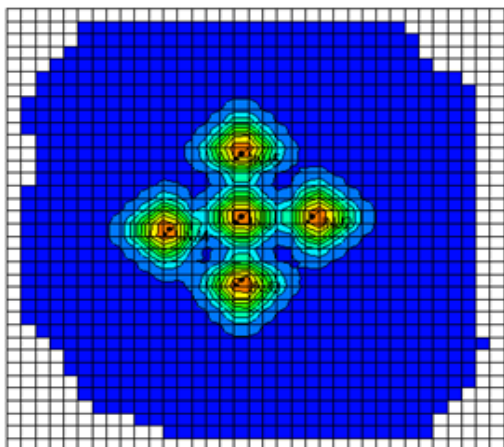
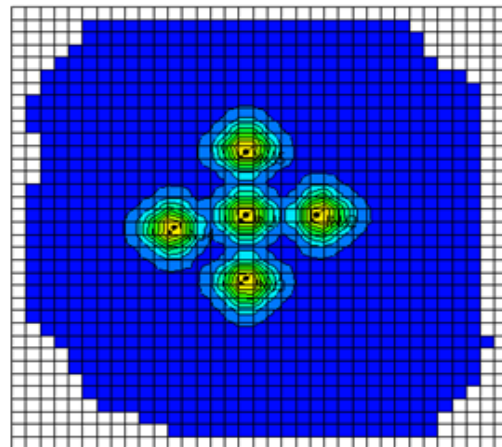
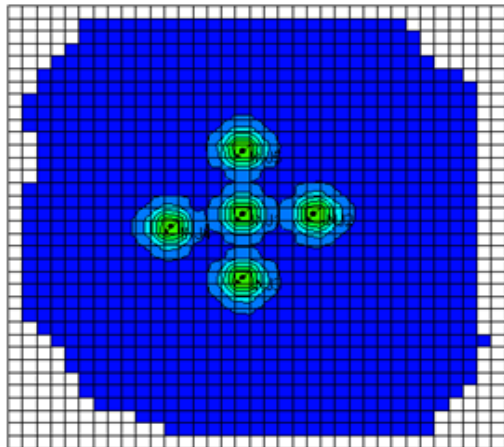
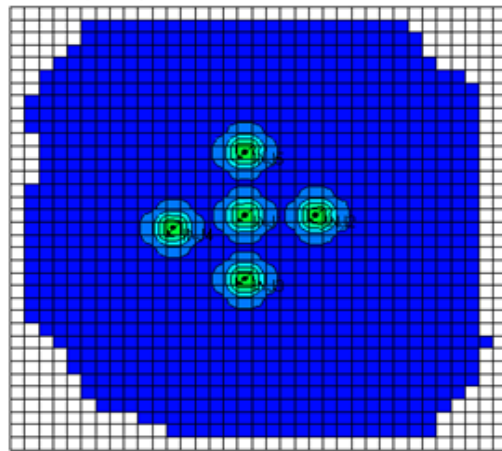
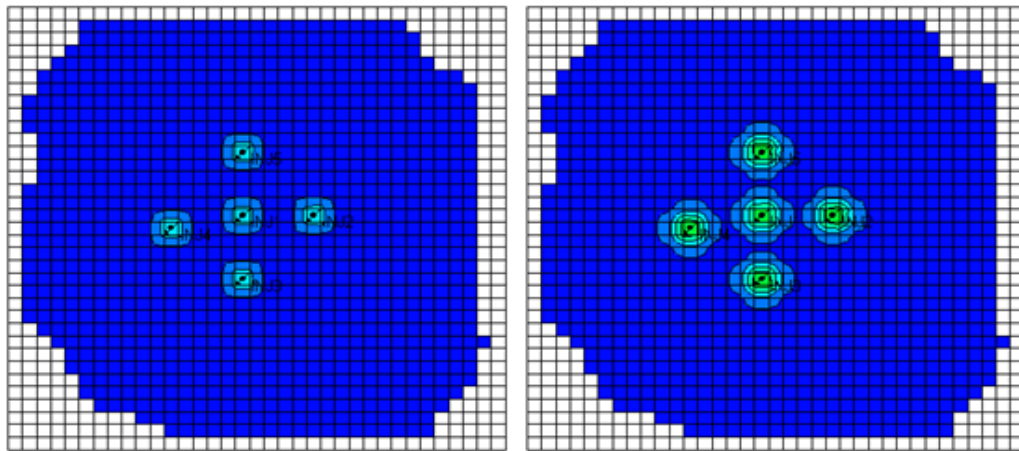
- ▶ Formation volume factor for CO<sub>2</sub> as 0.0048
- ▶ 9.194\*10<sup>10</sup>ft<sup>3</sup> CO<sub>2</sub> can be sequestered in the reservoir
- ▶ Two possibilities
  - ▶ Entire amount sequestered in the reservoir for nearly 4 years
  - ▶ Fraction of the captured amount

- ▶ When entire amount of CO<sub>2</sub> is sequestered
  - Using all five wells
  - Pressure crossed 7000 psia at the wells
  - Formation fracture risks

- ▶ A study was designed to inject CO<sub>2</sub> for a period of 10 years
- ▶ 38.24% of the captured amount (1.067 lbs/year)



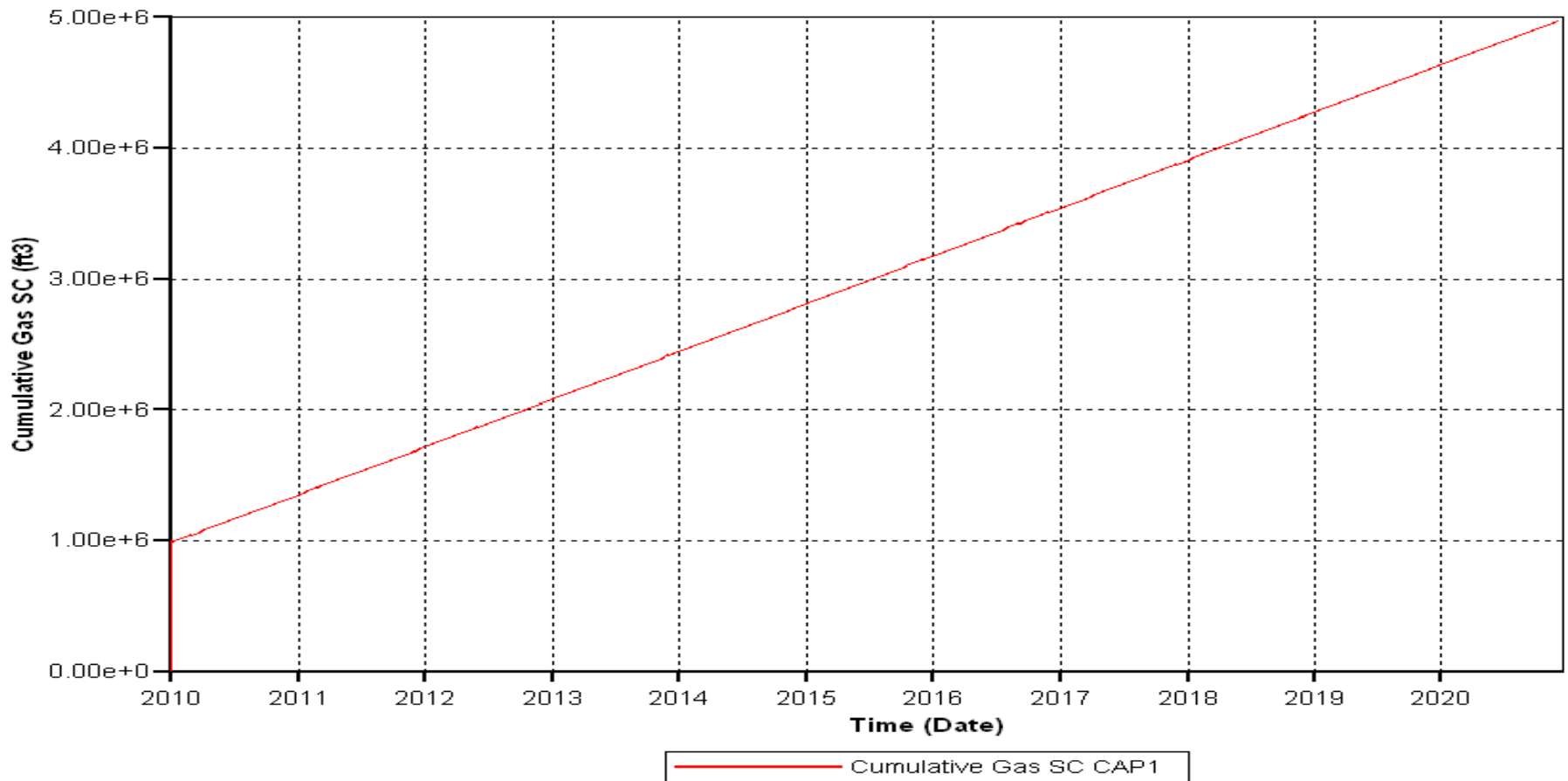
Global Mole Fraction(CO<sub>2</sub>)



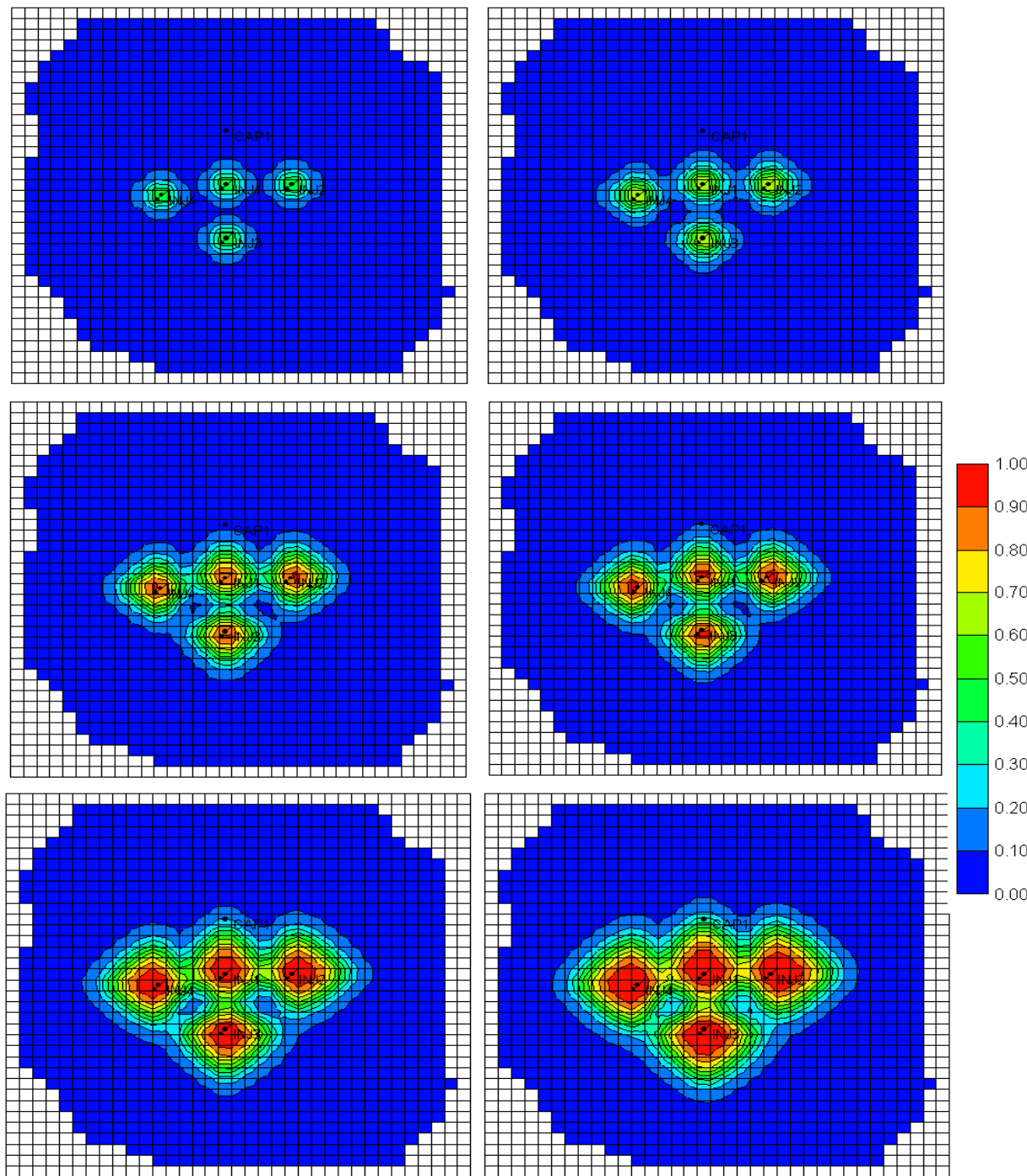
- ▶ CO<sub>2</sub> movement in the reservoir at various times
- ▶ Locations of the wells taken from literature

# Leakage effects

- ▶ One of the wells was assumed as an abandoned well and a pressure difference of 20 psia was assumed
  - $5.43 \times 10^{-3}$  percent of the total amount of CO<sub>2</sub> sequestered in the reservoir



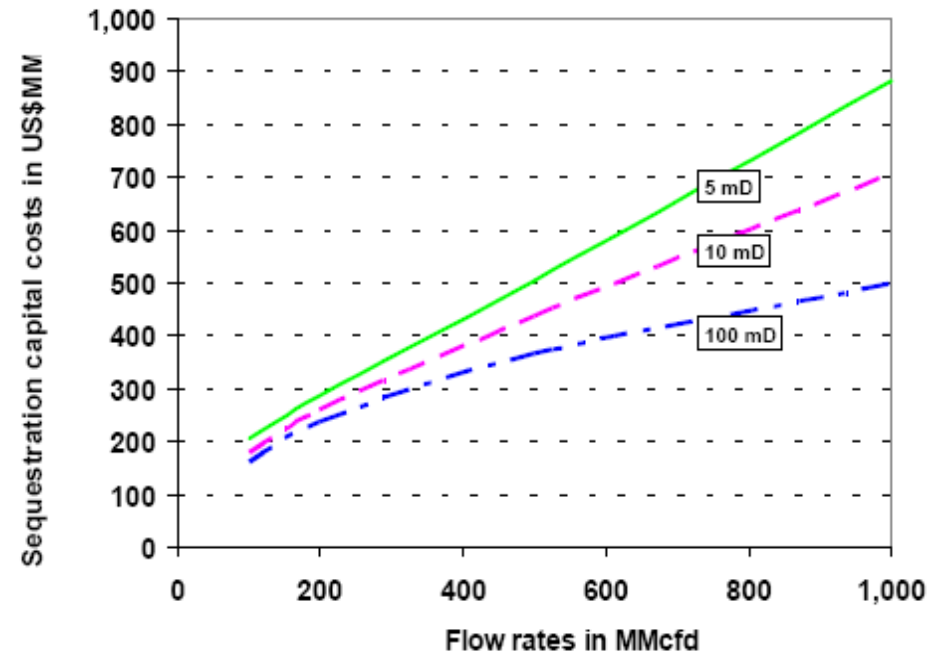
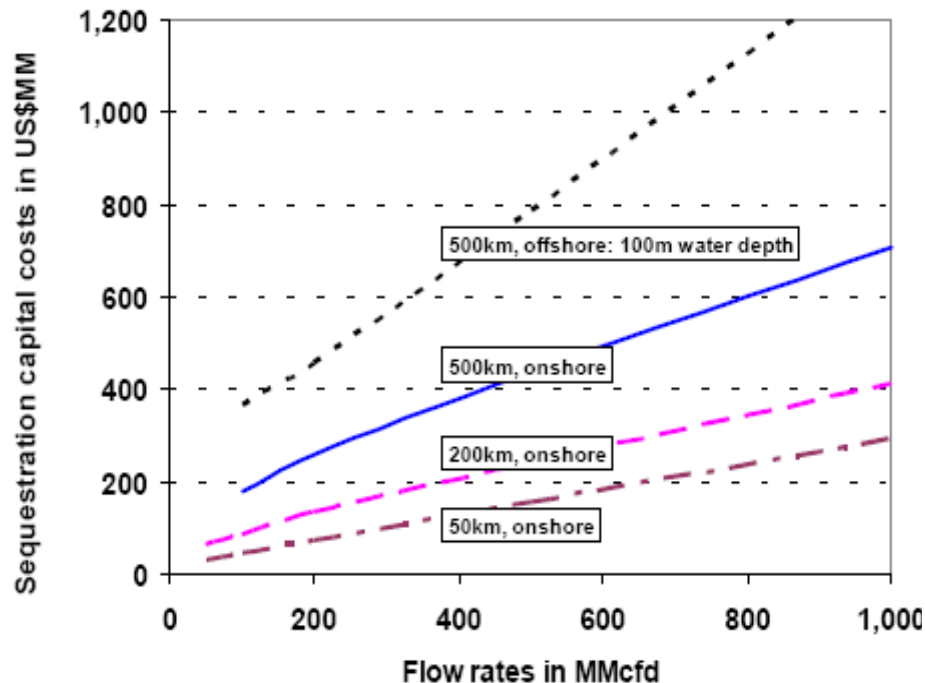
Global Mole Fraction(CO<sub>2</sub>) (with leakage)



- ▶ Properties are assumed to be homogeneous in a layer
- ▶ CO<sub>2</sub> movement should be identical
- ▶ Leakage dampens the movement profile and low pressure were observed in the region

# Economical analysis

- ▶ Site was assumed at a distance of 500 km
- ▶ Average permeability was calculated to find the overall capital cost
  - Average permeability is 111 mD
  - 100 mD curve was used
- ▶ Initial cost is \$290 millions



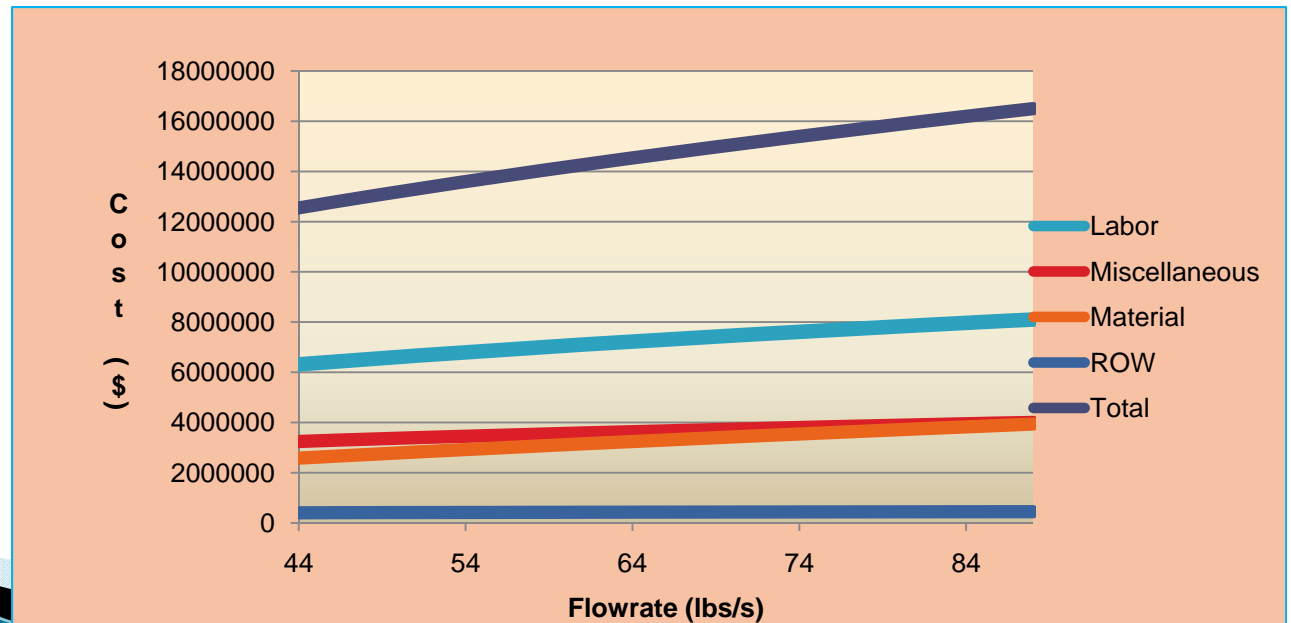
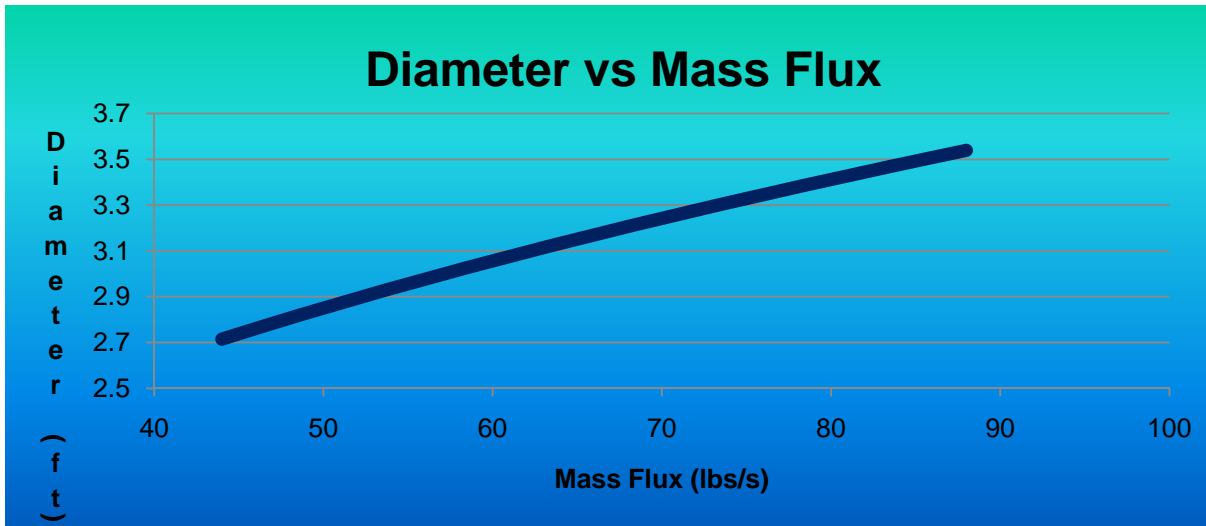


- ▶ No leasing costs were assumed
  - Exhausted oil field
- ▶ No Royalty cost
  - No production
- ▶ Operating cost is assumed to 10% of the cash flow
- ▶ Rate of return is assumed as 5% annually (0.0137% daily)

$$\frac{P}{A} = \frac{[(1+i)^n - 1]}{i(1+i)^n}$$

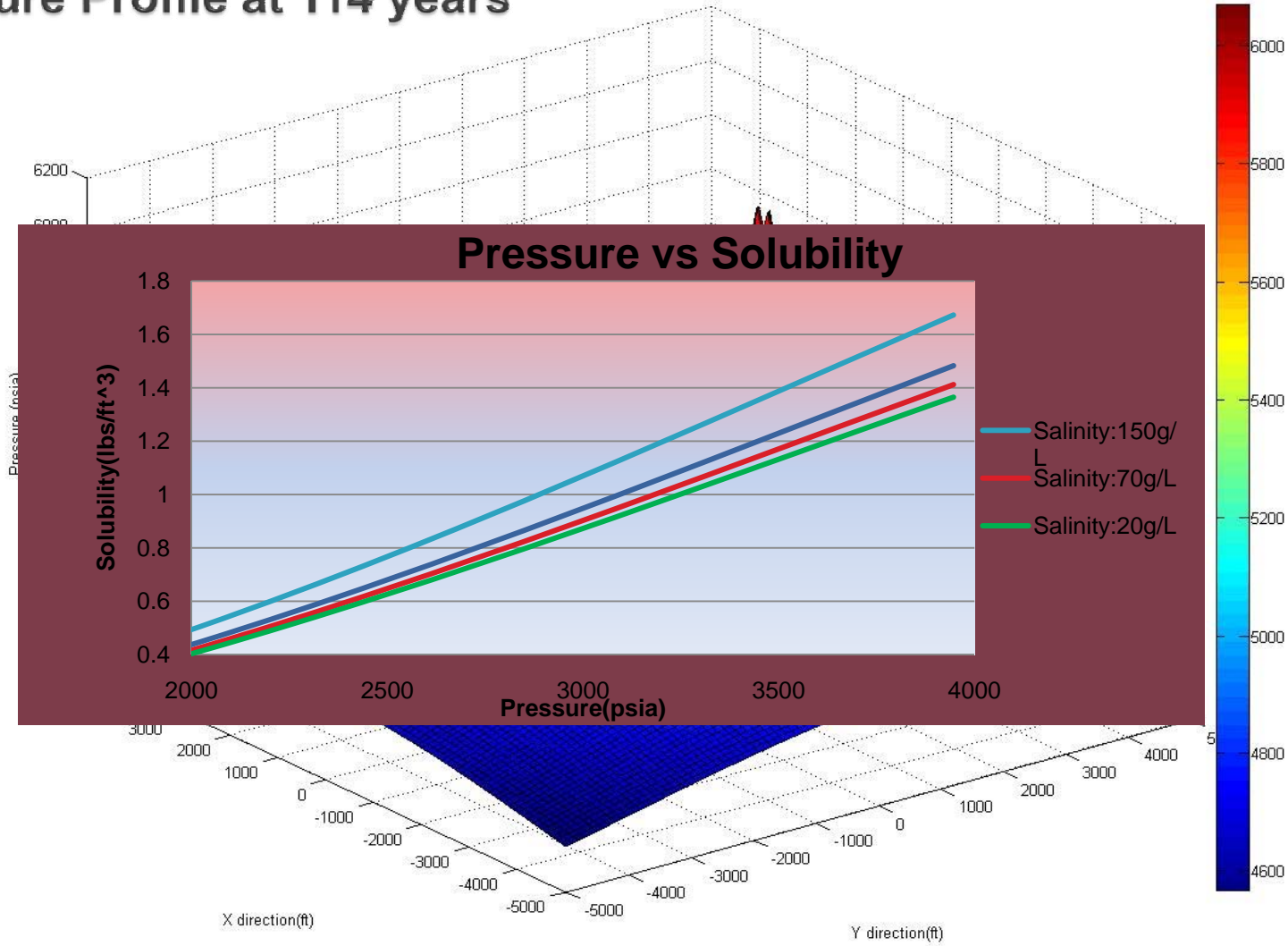
- ▶ Daily cash flow is found to be \$90526
- ▶ Cost for sequestration
  - \$0.4976/MSCF (or \$7.714/ton of CO<sub>2</sub>)

# CO<sub>2</sub> Sequestration In Saline Aquifers

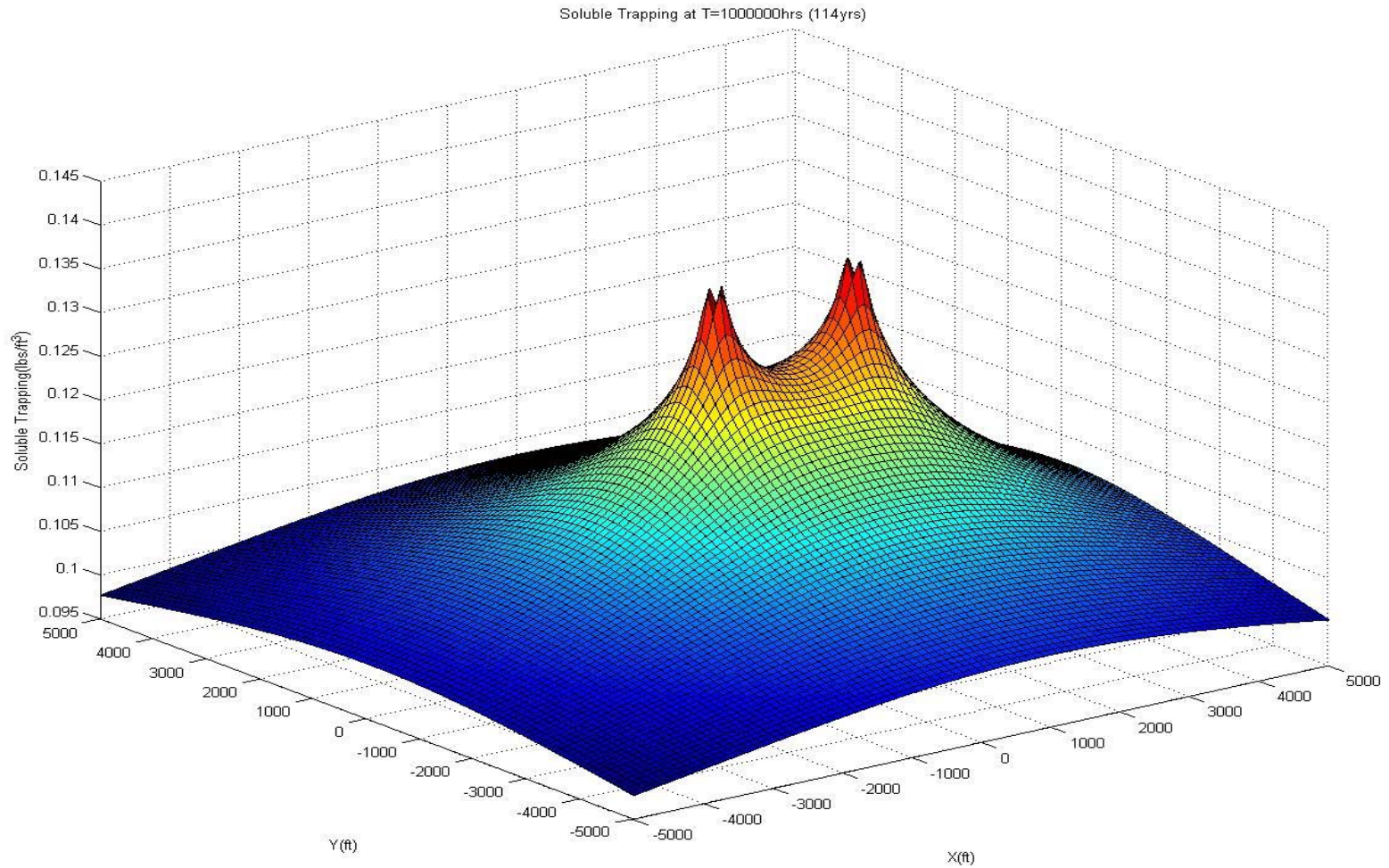


# Pressure Profile at 114 years

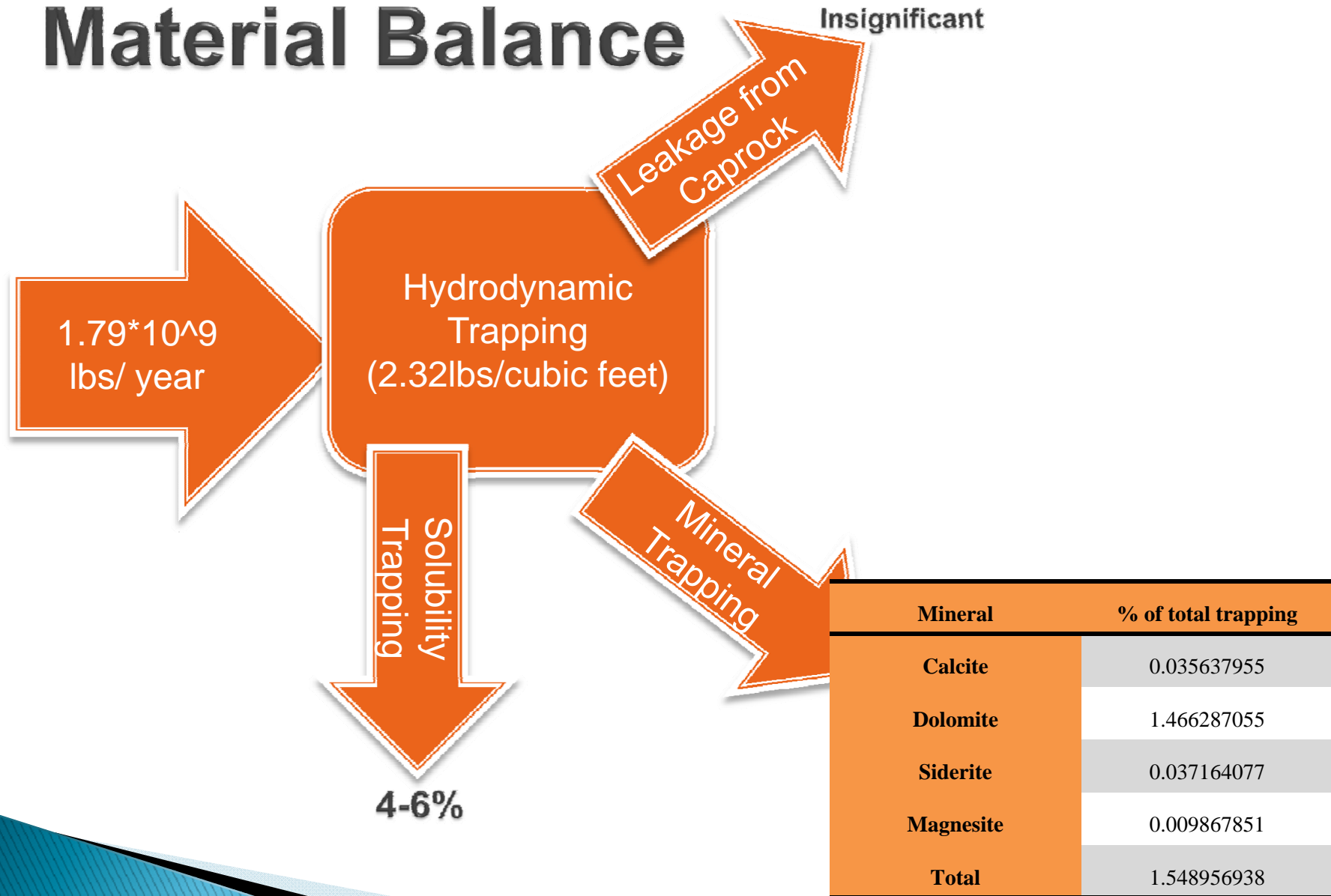
Pressure Profile when t:1000000 hrs (114 yrs)



# Solubility Trapping Capacity at 114 years



# Material Balance



Insignificant

Leakage from Caprock

$1.79 \times 10^9$   
lbs/ year

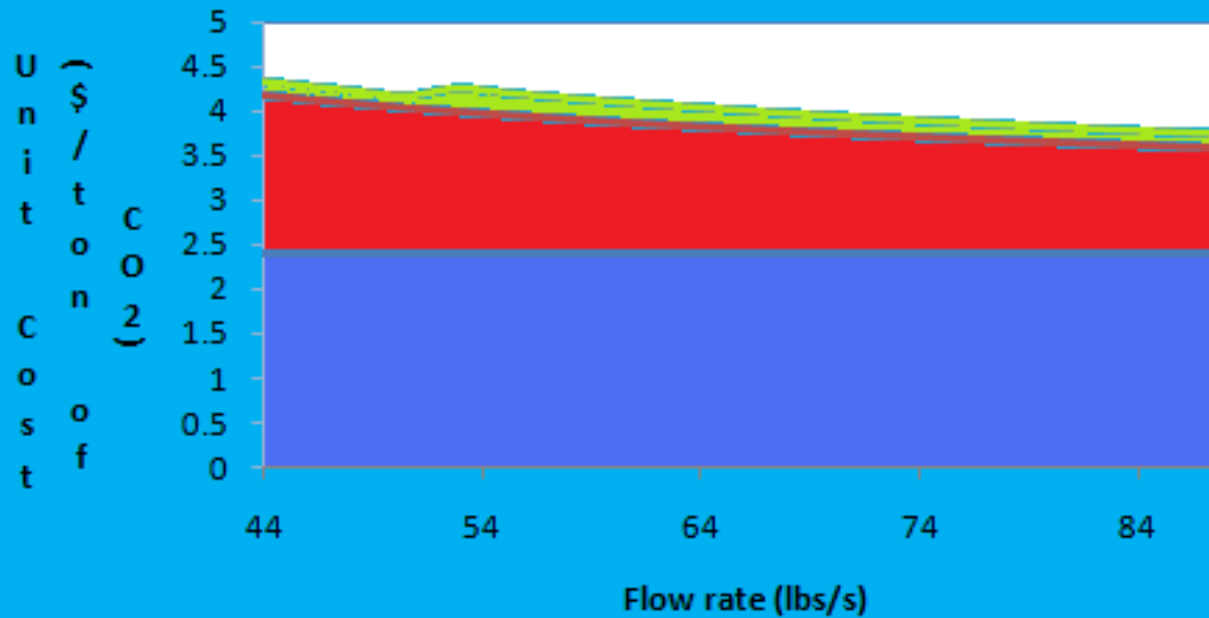
Hydrodynamic Trapping  
(2.32lbs/cubic feet)

Solubility Trapping  
4-6%

Mineral Trapping

Mineral	% of total trapping
Calcite	0.035637955
Dolomite	1.466287055
Siderite	0.037164077
Magnesite	0.009867851
Total	1.548956938

# Unit Cost vs. Flow Rate



- Compression Cost
- Transportation Cost
- Cost of Wells

**Questions?**

